# A future "CO<sub>2</sub> Free" Power Plant for Coal Technology and Economics

The annual fall meeting of the German Physical Society Bad Honnef, October 21-22, 2004

### Lars Strömberg

Vattenfall AB Group Function Strategy Berlin/Stockhom



© Vattenfall AB

Lars Stromberg 2004

### 2 The Vattenfall Group

- Vattenfall is one of the major Energy companies in Europe
- Vattenfall sells about 180 TWh electricity
  - The main part is produced by hydropower, nuclear power, coal and natural gas.
  - A smaller part is produced by biofuels and wind power
  - About 17 TWh is produced in combined heat and power plants
- Vattenfall also sell about 37 TWh heat
  - The main part is produced by biofuels, coal and gas in cogeneration plants
- Vattenfall emits almost 80 million tons of CO<sub>2</sub> per annum



### **Power Plant Lippendorf**





© Vattenfall AB

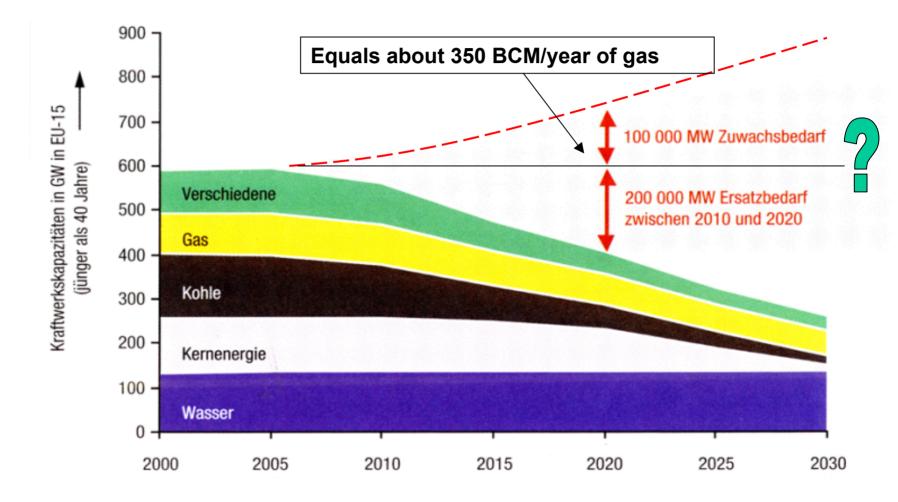
CO<sub>2</sub> free power plant

# Fossil fuels are needed



© Vattenfall AB

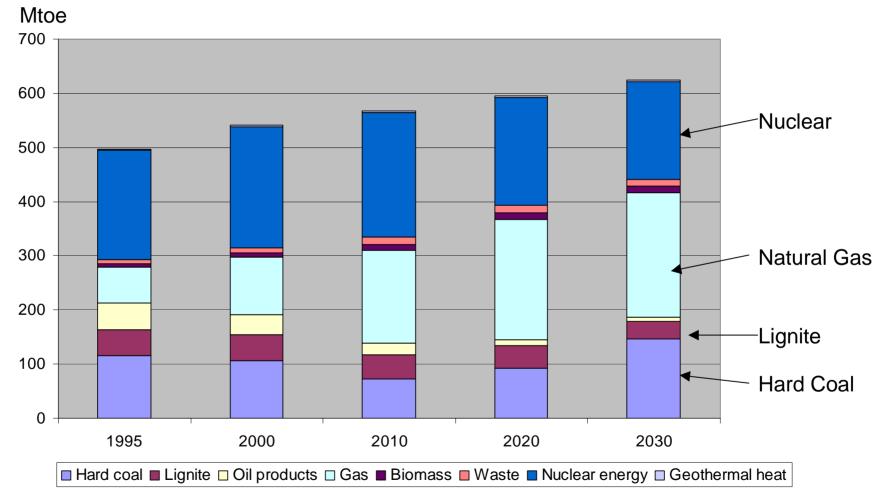
### 5 Need for new capacity in Europe (EU 15)



Source: VGB PowerTech Annual Report 2002 / 2003 + EU and Eurelectric Lars Stromberg 2004



### **Fuel use for electricity generation EU-15**



Source EU Commission Energy and Transport Outlook 2030 (2003)



### Fossil fuels – an essential part of our society

Today, fossil fuels are completely dominant in world wide energy supply. World Energy Outlook 2002:

- "Global primary energy demand is projected to increase by 1.7% per year from 2000 to 2030. Fossil fuels will remain the primary sources of energy, meeting more than 90% of the increase in demand"
- According to the Green Paper on Energy Supply, 80% of the energy consumption in EU-30 derives from fossil fuels:

EU 30	Today	2030
Fossil fuels	80%	85%
Nuclear	15%	6%
Renewables	<b>6%</b>	8%



**CO<sub>2</sub> free power plant** 

# The big challenge for Coal is the CO2 issue



© Vattenfall AB

# 9 Kraftwerk Boxberg





### 10The challenge for Coal

#### Coal is a very good fuel .....

- It is very easy to burn and it is safe to store and transport
- The cost is low and stable. It costs less than half compared with gas and it is available all over the world.

#### Modern technology allow us to....

- Eliminate almost all emissions of "conventional" pollutants as sulfur and nitrogen oxides, hydrocarbons and particulates, it is only a matter of cost.
- Get a very high efficiency (over 45 %)If the trading system prevails



The big challenge for Coal is the carbon dioxide emission. If this can be eliminated we can utilize coal with confidence without endangering the Climate



# Emission Trading sets the commercial framework for new technology

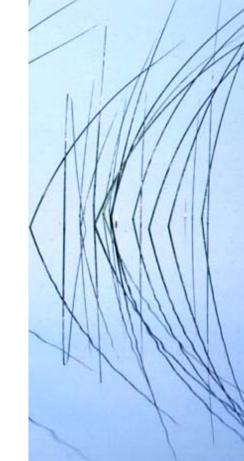


### The EU scheme for GHG emission trading

"The Directive establishes a scheme for greenhouse gas emission allowance trading within the European Community to promote reductions of greenhouse gas emissions in an economically efficient manner".

Adopted by European Parliament 2 July 2003

Sept 2003: Adopted by European Council March 2004: National Allocation Plans Sept 2004: Allocations fixed January 2005: Effective First period: 2005-2007 Second period: 2008-2012





The long term price of the allowances will be set by reduction requirements and the costs of physical reduction

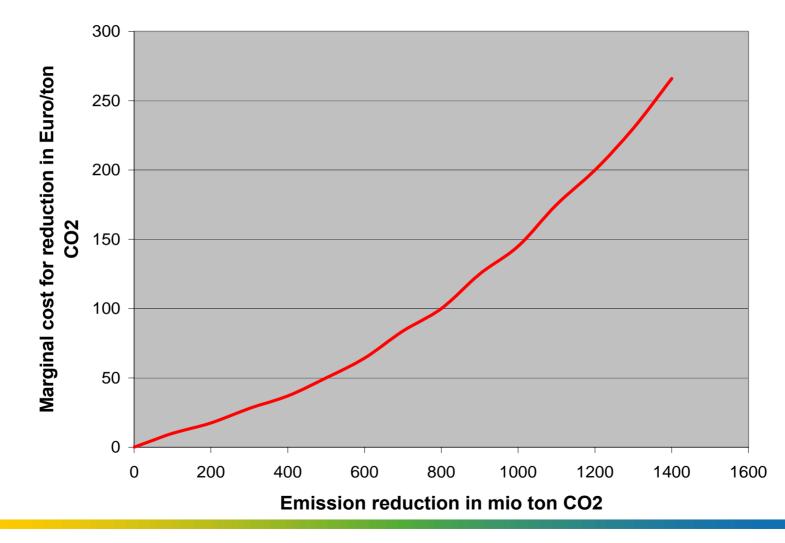
# As emission allowances become scarce they will have an increasing value

The cost for allowances will be added as a direct marginal production cost and therefore increase the spot price of electricity



#### Marginal cost vs. Reduction of CO2 emissions in EUR/ton CO2

Source: ECOFYS Economic evaluation of sectorial reduction objectives for climate change





Lars Stromberg 2004

# 15 **Analyses show that...**

### by 2010 .....

- Costs for emission allowances might be around 10 EUR/ton of CO2

#### but in 2015....

- If the trading system prevails
- When new technology for fossil fuels with near zero emissions, can play a significant role
- The cost for emission allowances will increase to  $20 \text{ EUR/ton of CO}_2$  or higher depending on reduction demand.



This is the target to be met by new "zero emission" technology



**Capture and storage of CO<sub>2</sub>** 

# Capture and storage



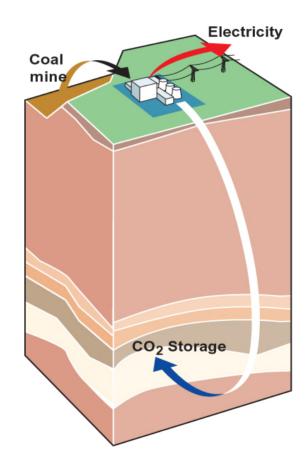
© Vattenfall AB

### **The CO<sub>2</sub>-free Power Plant principle**

The principle of capture and storage of the  $CO_2$  under ground

The  $CO_2$  can be captured either from the flue gases, or is the carbon captured from the fuel before the combustion process.

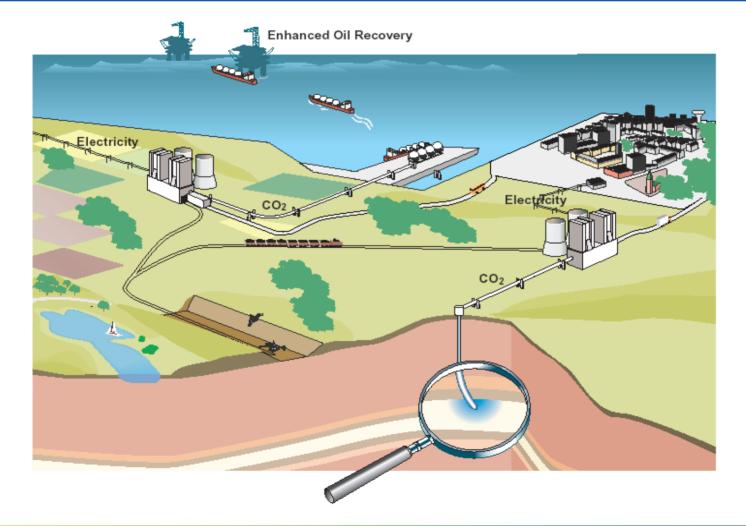
The CO2 is cleaned and compressed. Then it is pumped as a liquid down into a porous rock formation for permanent storage.





© Vattenfall AB

### 18 CO<sub>2</sub> Capture and storage





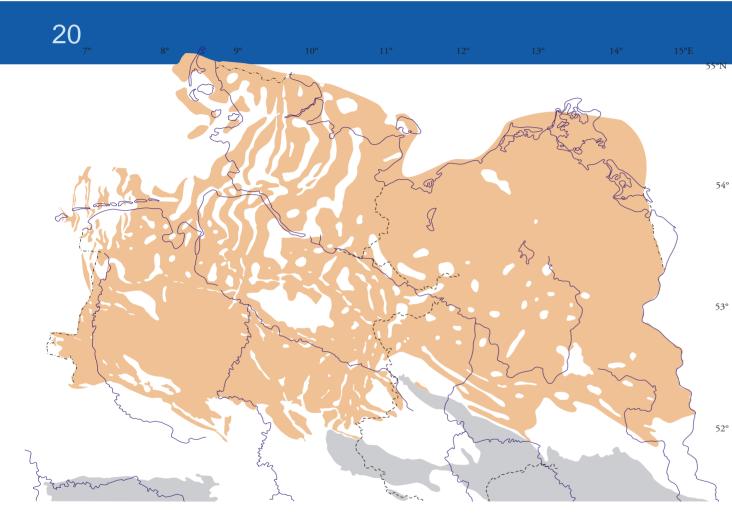
19 **CO<sub>2</sub> free power plant** 

# Storage



Lars Stromberg 2004

## **Storage Capacity, saline aquifers**



#### Specific problems:

- structurally complex
- thickness variation
  - porosity variation
  - residual saturation

Source: Franz May, Peter Gerling, Paul Krull Bundesanstalt für Geowissenschaften und Rohstoffe, Hannover



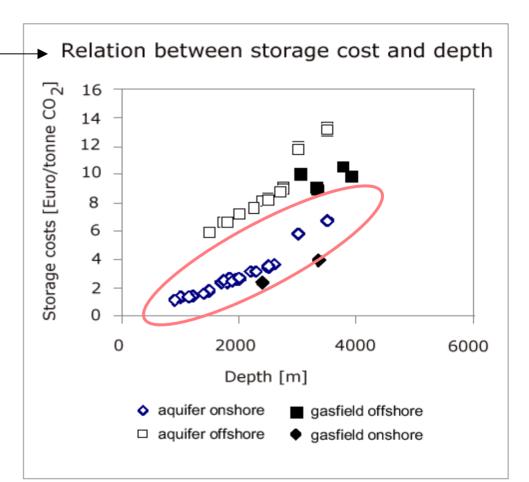


### **Storage cost estimates**

#### Storage in aquifer traps (GESTCO Figures)

- Costs depend strongly on the depth of subsurface layers used for storage
- The strongest subsurface uncertainty in storage costs lies in the time it takes to fill the trap
- The second important uncertainty parameter is the exploration success ratio of finding a suitable trap
- Dutch case: CO2 source of 5.7 Mton/year stored in one megatrap or a conglomerate of traps. Total sequestration cost: 17-20 Euro/ton CO2 av.

Källa: Christian Bernestone Vattenfall Utveckling





22 CO<sub>2</sub> free power plant

# Transport

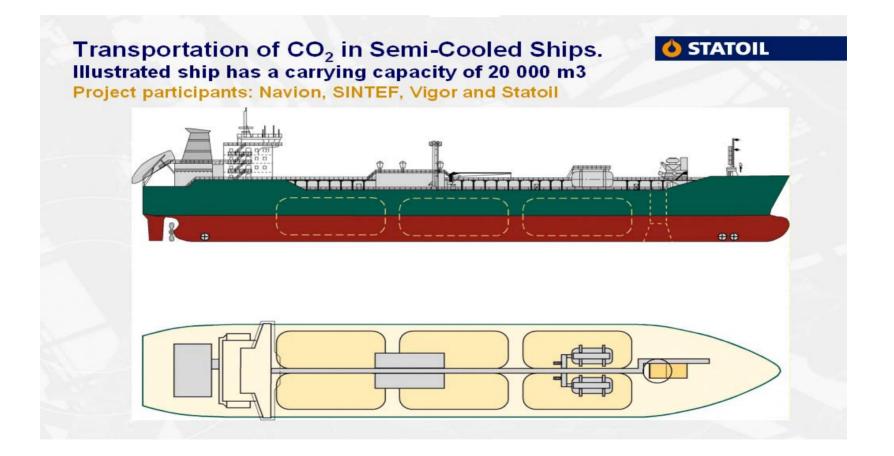


## 23 **CO<sub>2</sub> pipelines in operation in the USA**





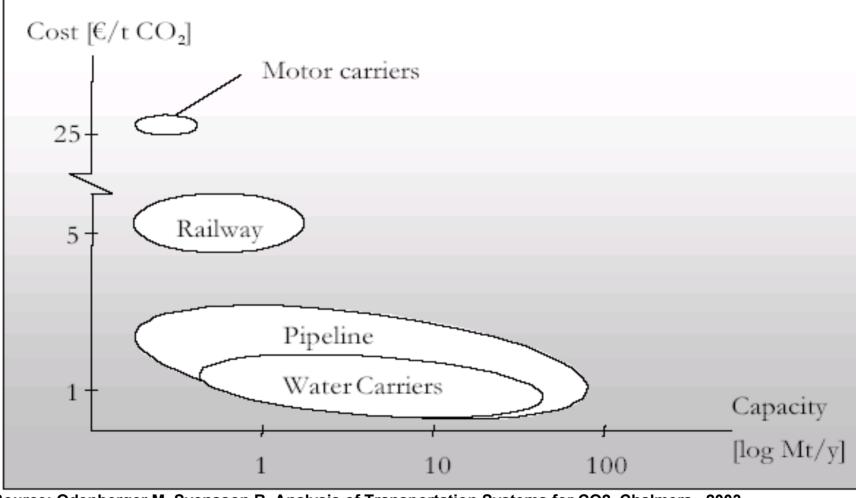
### Transportation with water carriers





© Vattenfall AB

### **Transport costs for CO2** Cost and capacity ranges



Source: Odenberger M, Svensson R, Analysis of Transportation Systems for CO2, Chalmers, 2003



© Vattenfall AB

26 CO<sub>2</sub> free power plant

# Capture



© Vattenfall AB

Lars Stromberg 2004

# Different ways to capture the CO2 – minimize costs



## CO<sub>2</sub> free power plant - Capture

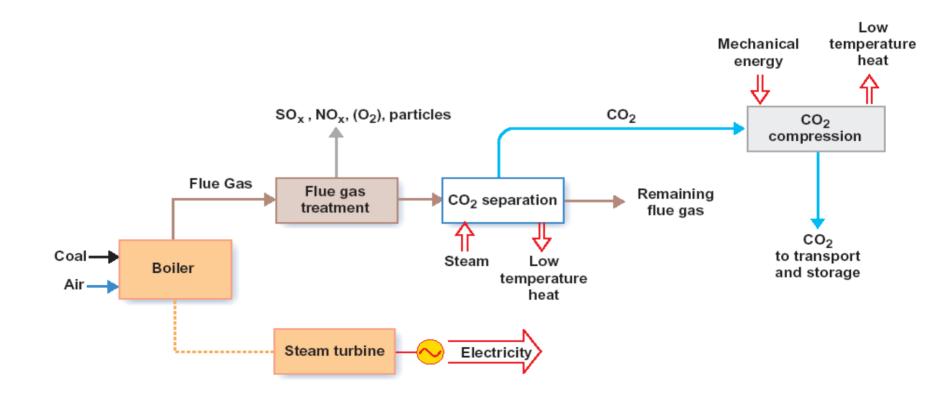
- Reasonably matured technologies for capture of CO<sub>2</sub> are usually divided in three categories
  - Post-combustion capture, where the flue gas from the combustion is cleaned from  $CO_2$ .
  - Pre combustion capture, where the carbon is removed from the fuel before the combustion.
  - Utilization of oxygen for the combustion, but without the nitrogen in air, in form of either air separation or a solid oxygen carrier

Vattenfall works with all three options, but we have made an agreement with our collegues to share the workload and share results

© VattenfaltrABberg	2003 07 05
Vattenfall AB	Lars Stromberg 2004
Corporate Strategies	

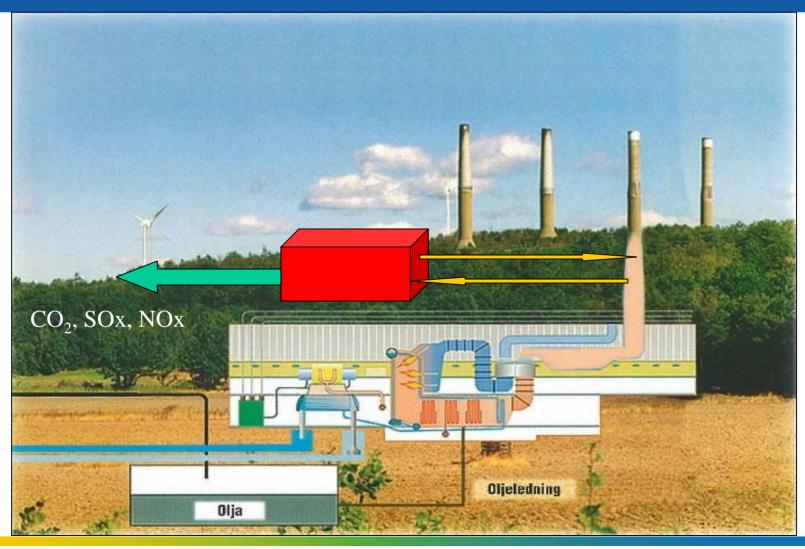


### **Post-combustion capture – absorption process**



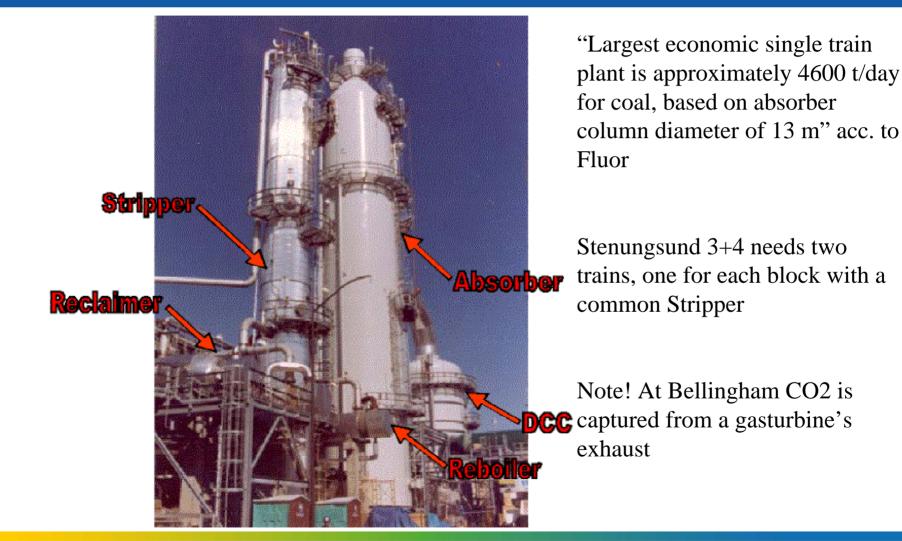


### **Stenungsund - The Power plant inside the mountain**



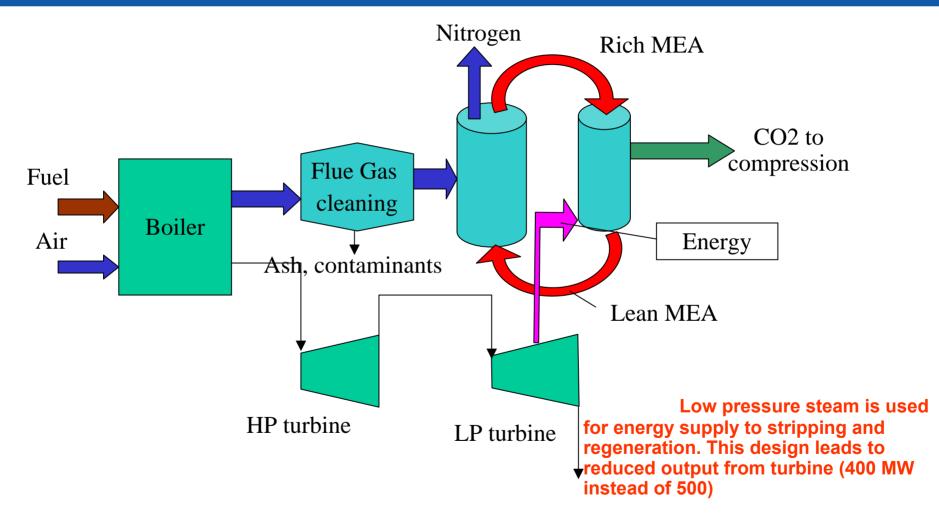


### 31 **Bellingham Plant, CO<sub>2</sub> absorption**





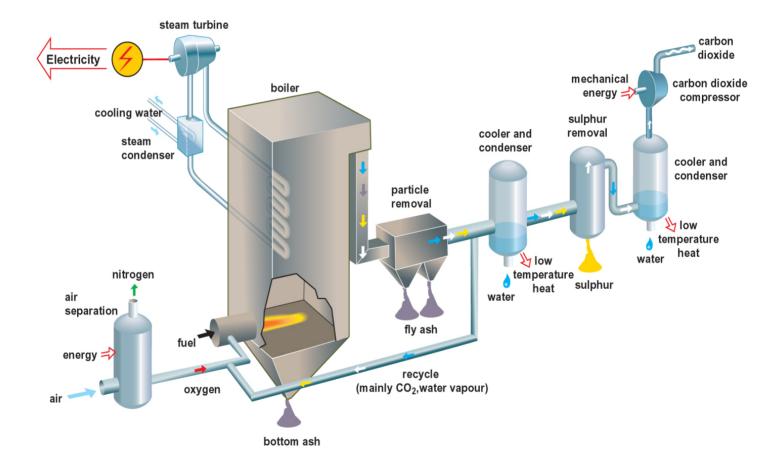
### Amine Absorption process principle





© Vattenfall AB

### $O_2/CO_2$ combustion is the preferred option at present



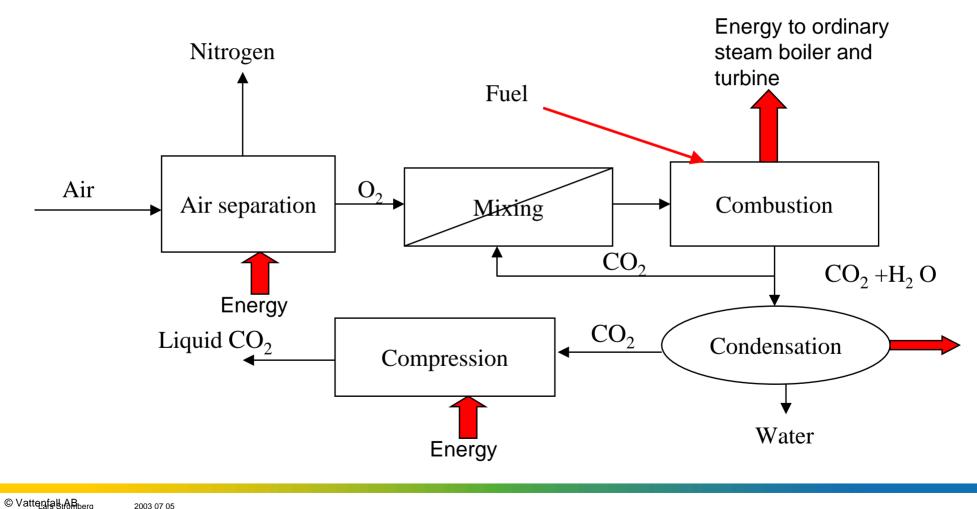


### <sup>34</sup> The reference power plant Lippendorf





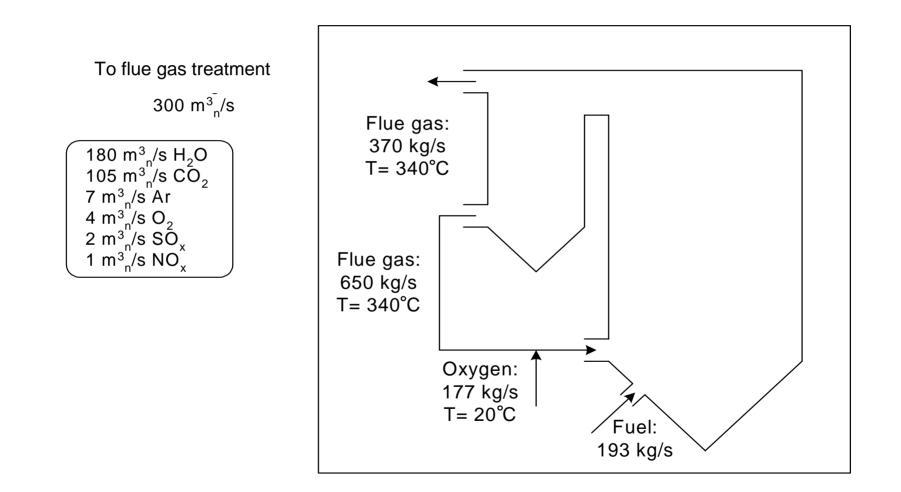
### 35 $CO_2$ free power plant : $O_2/CO_2$ combustion





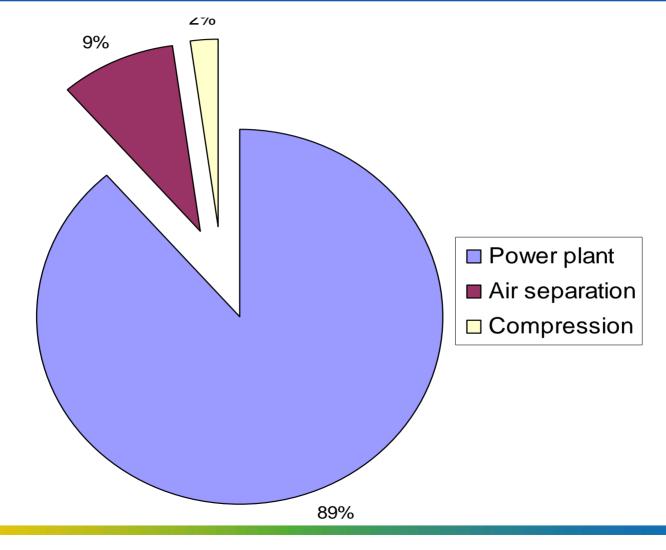
© Vattenfall AB Lars Stromberg 2004 Corporate Strategies

#### 36 The gas flows in the boiler if fed with an oxidizer with 21% O2

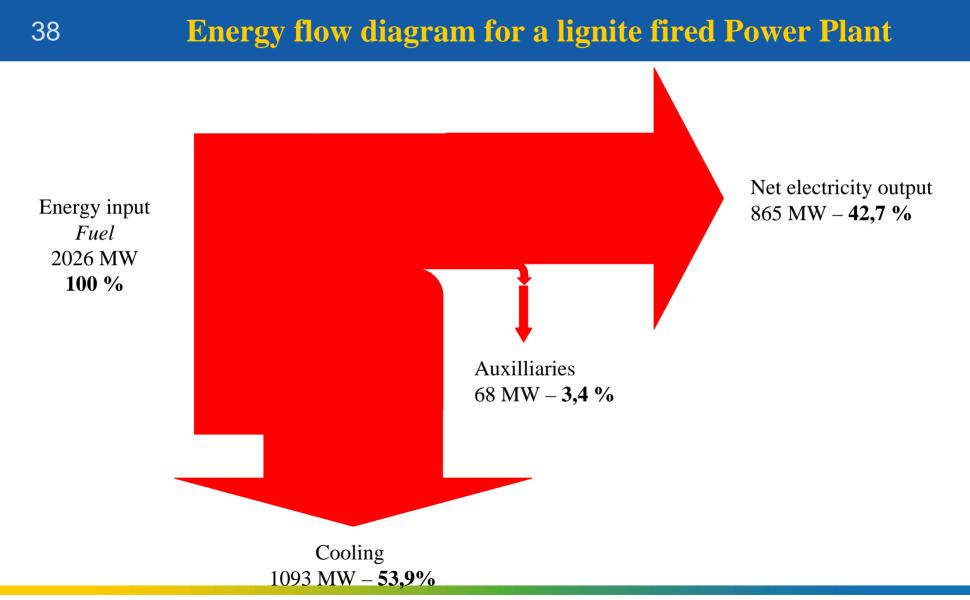




# 37 Investment cost for a large lignite fired power plant with O<sub>2</sub>/CO<sub>2</sub> combustion

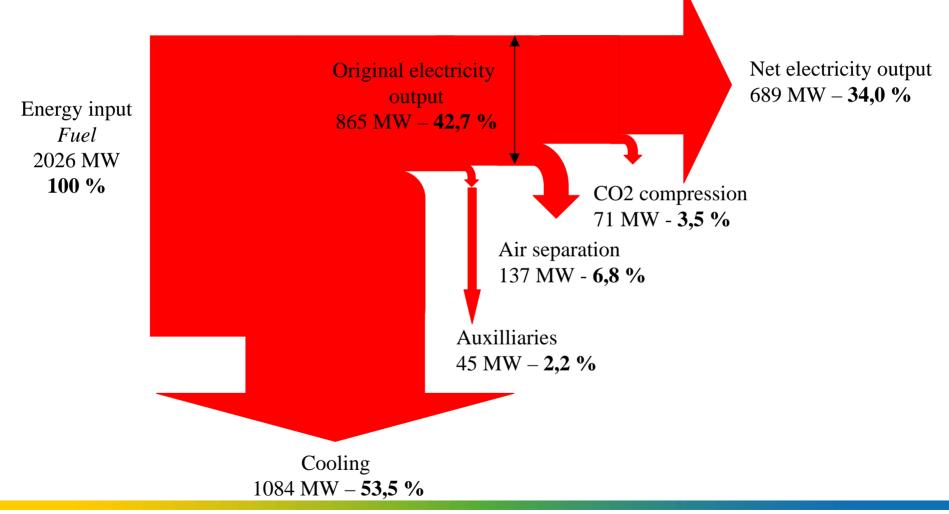








#### 39 Energy flow diagram for lignite fired plant with $O_2/CO_2$ combustion





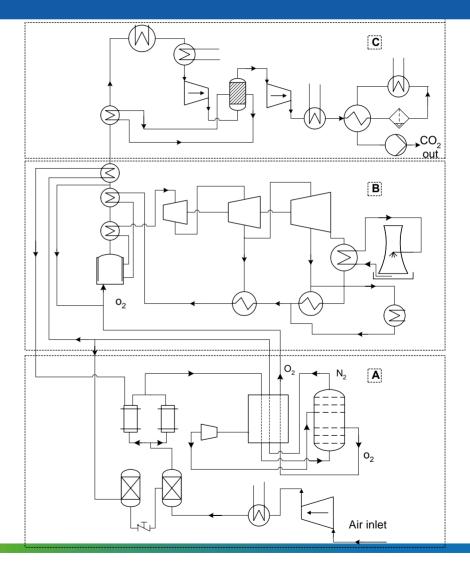
Lars Stromberg 2004

#### 40 The process design of the O2/CO2 power plant

Flue gas treatment and liquifaction of the CO2. Power consumption –71 MW

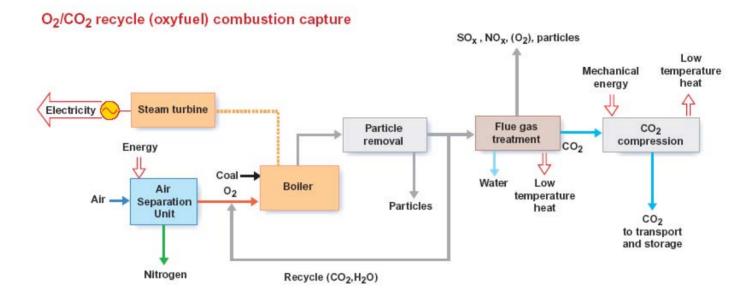
The power plant process. Original gross output 933 MW

Air separation Power Consumption -141 MW





## The CO<sub>2</sub>/O<sub>2</sub> combustion principle



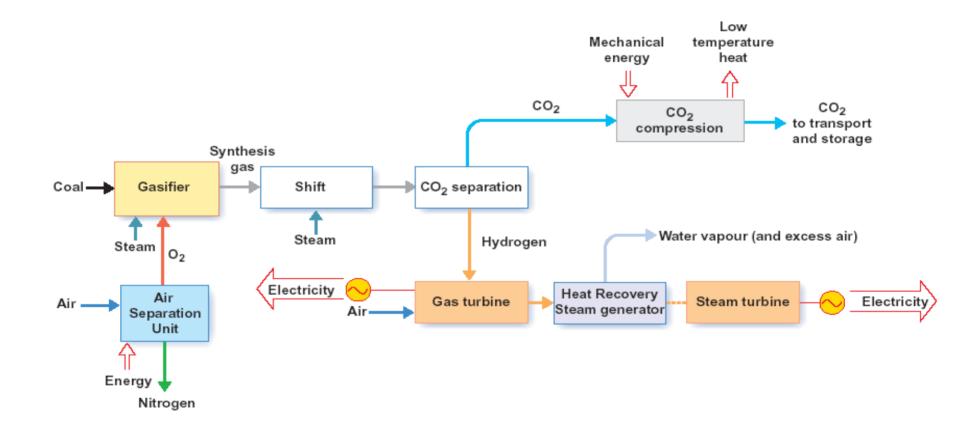
Large energy penalty for  $O_2$  production

Large amount of waste heat, not only from steam condenser but also from flue gas condenser and  $CO_2$  compression



© Vattenfall AB

#### 42 **Pre-combustion - decarbonisation capture**





43 CO<sub>2</sub> free power plant

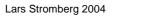
# Evaluation of the options



#### CO<sub>2</sub> Capture Evaluation of options

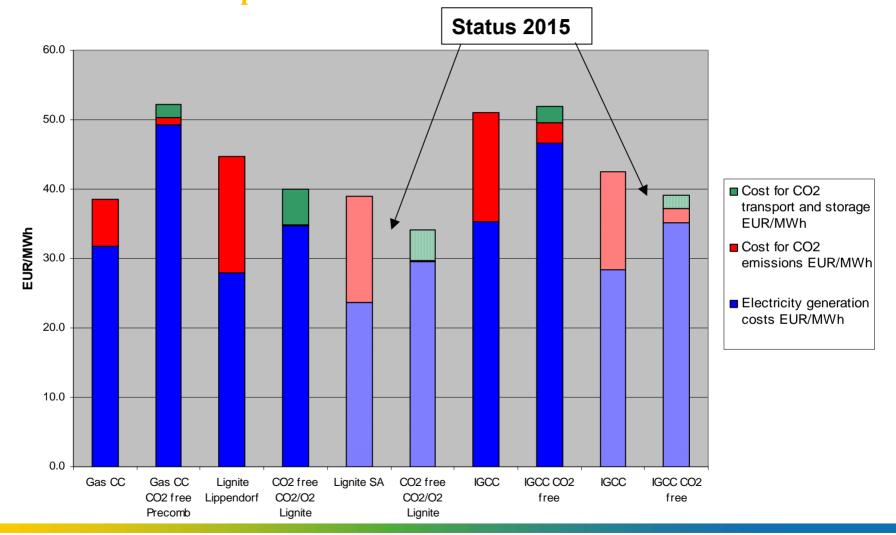
	Gas CC	Gas CC CO2 free Precomb	Lignite Lippendorf	CO2 free CO2/O2 Lignite	Lignite SA	CO2 free CO2/O2 Lignite	IGCC	IGCC CO2 free	IGCC	IGCC CO2 free
Reference	Sintef	Sintef	VAB	VAB	VAB	VAB	IEA	IEA	IEA	IEA
Fuel	Gas	Gas	Lignite	Lignite	Lignite	Lignite	Coal	Coal	Coal	Coal
Power output MW	400	392	865	700	500	500	776	676	750	700
Specific Investment cost EUR/kW	625	1430	1272	1570	1005	1366	1371	1860	900	1250
Efficiency %	60	49	42,7	34,3	47	39,8	43,1	34,5	48	43,2
Fuel cost EUR/MWh fuel	12,5	12,5	4	4	4	4	5,8	5,8	5,8	5,8
O&M cost EUR/MWh	2,7	5,8	4,0	5,0	3,4	3,9	6,7	9,5	6,0	7,8
CO2 emitted kg/MWh	335	53	836	7	760	4	786	142	706	102







#### **CO<sub>2</sub> Capture** Evaluation of options





45

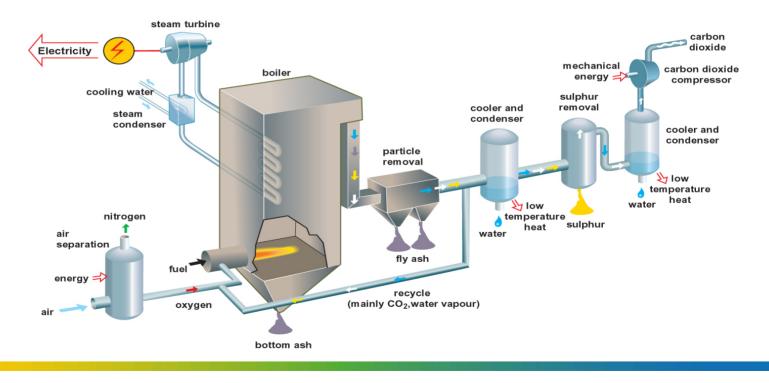
#### **Opportunities with oxyfuel combustion**

- Based on existing boiler and steam cycle technology
  - Can take advantage of ongoing development to increase efficiency of conventional power plants, e.g. AD700
- Co-capture of CO<sub>2</sub> and other pollutants gives a near zero emission power plant
  - Reduction in cost of flue gas treatment
- Next generation novel boiler designs
  - Compact PF boiler design through low recycle rate (higher oxygen concentration)
  - CFB gives opportunity to even lower recycle rate through use of solids for heat transfer

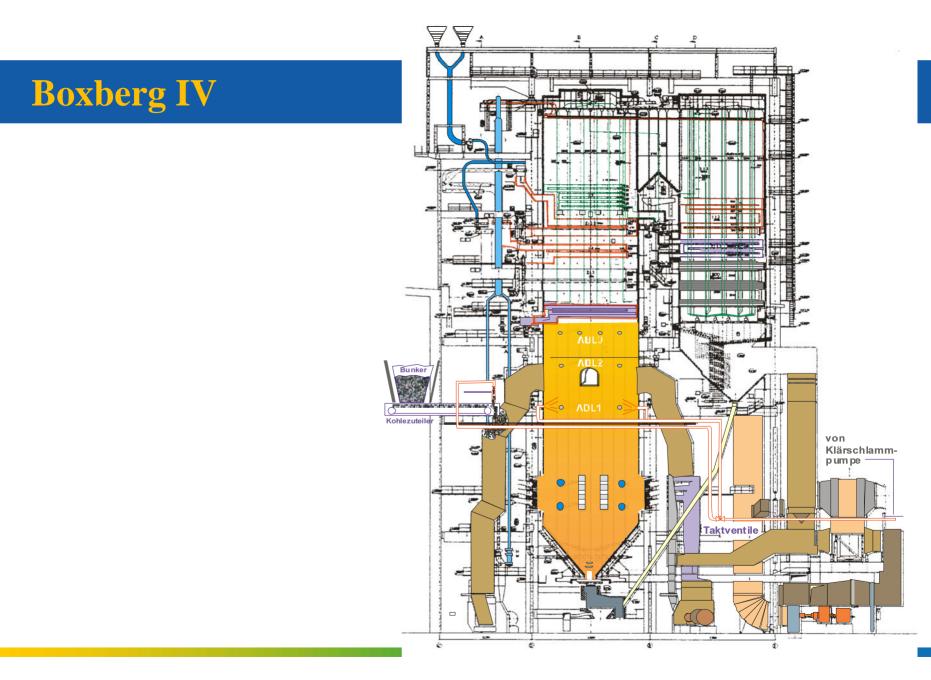


#### 47 **Challenge 1: Boiler design**

- Design of next generation oxyfuel boiler, combustion considerations
- Reduced recycle rate or complete removal of recycle
- Optimisation of combustion for reduced formation of NO<sub>x</sub>, to eliminate catalytic reactors









#### 49 **O**<sub>2</sub> /CO<sub>2</sub> combustion – experiments and modeling

Modeling of an experimental CO2/O2 flame

23 % oxygen + CO2+H2O

**1300 Celcius** 



#### Combustion in a CO<sub>2</sub>/H<sub>2</sub>O rich atmosphere

A number of parameters vary when combustion takes place with CO2/O2 instead of air as oxidizer

> Transport properties Thermal & radiative properties Volumetric flow rates Combustion kinetics Ash character

→Heat release rate

- → Flame temperature
- →Heat fluxes
- →Thermal performance

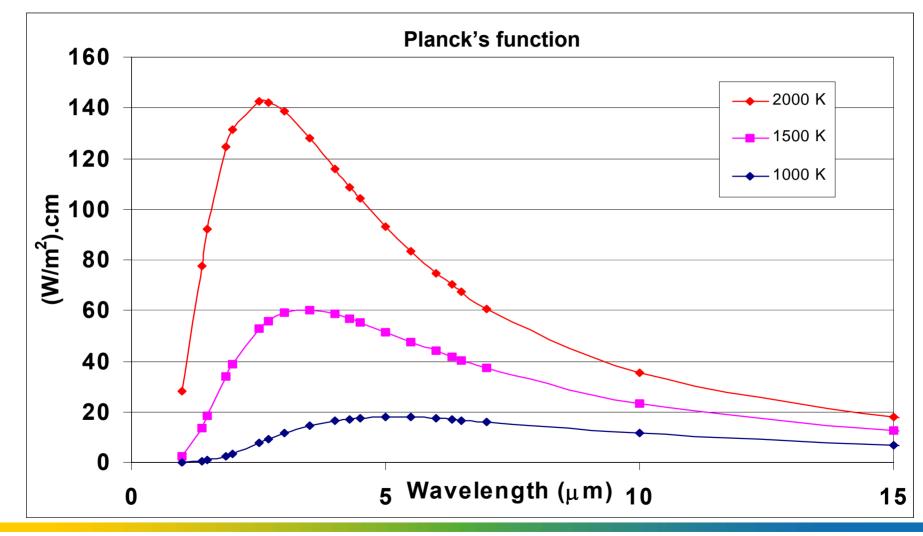
Some figures honestly stolen from: Raj Gupta

# *The* University *of* Newcastle &





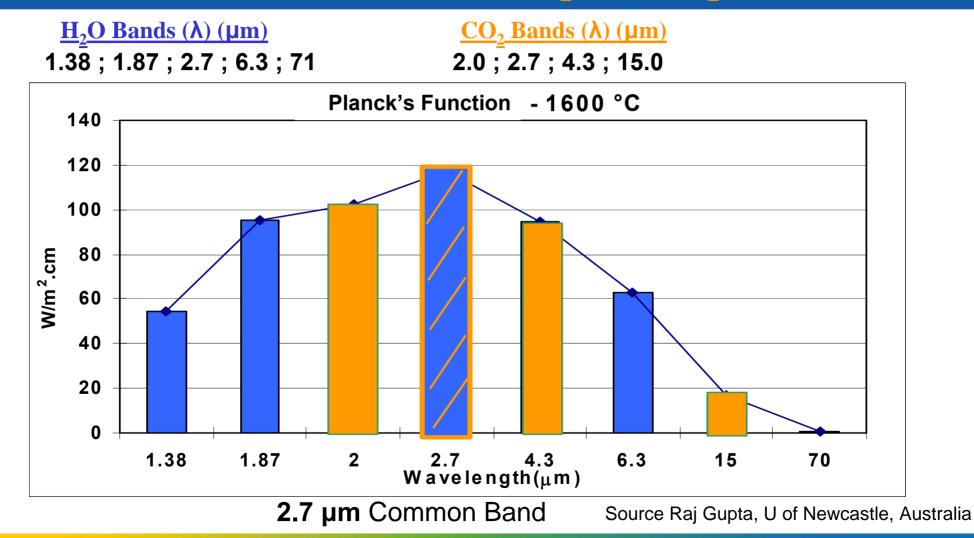
#### 51 Planck's Distribution Function – H<sub>2</sub>O & CO<sub>2</sub> Bands





Lars Stromberg 2004

#### 52 **Principle Emission Bands:** H<sub>2</sub>O & CO<sub>2</sub>





Total emissivity of gray gases:

Lars Stromberg 2004

Source Raj Gupta, U of Newcastle, Australia

i

VATTENFALL

k PS

 $a_{\varepsilon,i} = \sum_{j=1}^{j} b_{\varepsilon,i,j} T^{j-1} \qquad i=3 \text{ (no. of gray gases)}$ 

i

3-gray gas model

i

**Optimized values for:** 

**j** = 4 (polynomial order)

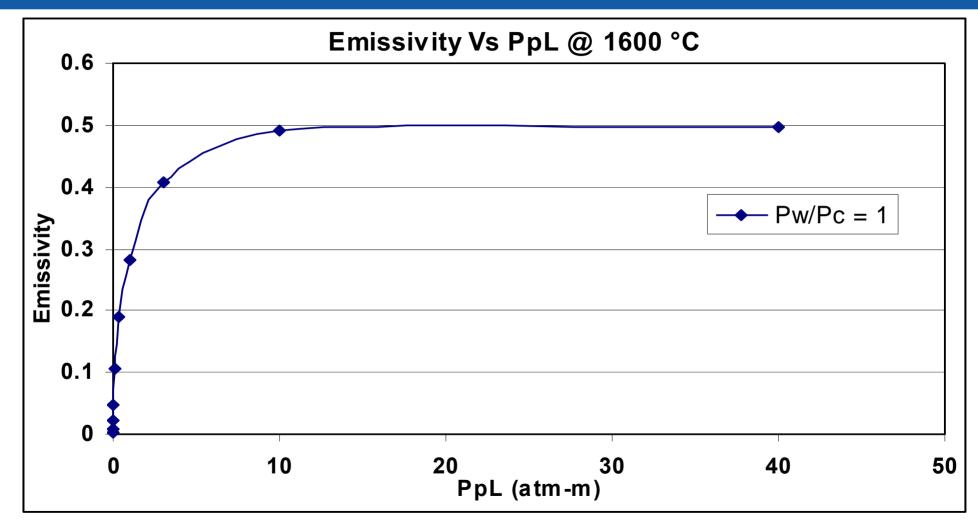
Where,  

$$a_{\varepsilon,i} = i^{th} gray gas emissivity weighting factors$$
  
 $\begin{bmatrix} k & PS \end{bmatrix} th$   
 $\boxed{S}$  (Partial pressure \* Path Length ) of absorbing gas  
 $b_{\varepsilon,i,j} = emissivity$  gas temperatur e polynomial coefficien ts

Article: T.F.Smith et al (1982)



#### 54 WSGGM – Emissivity Vs PpL – 1600 °C



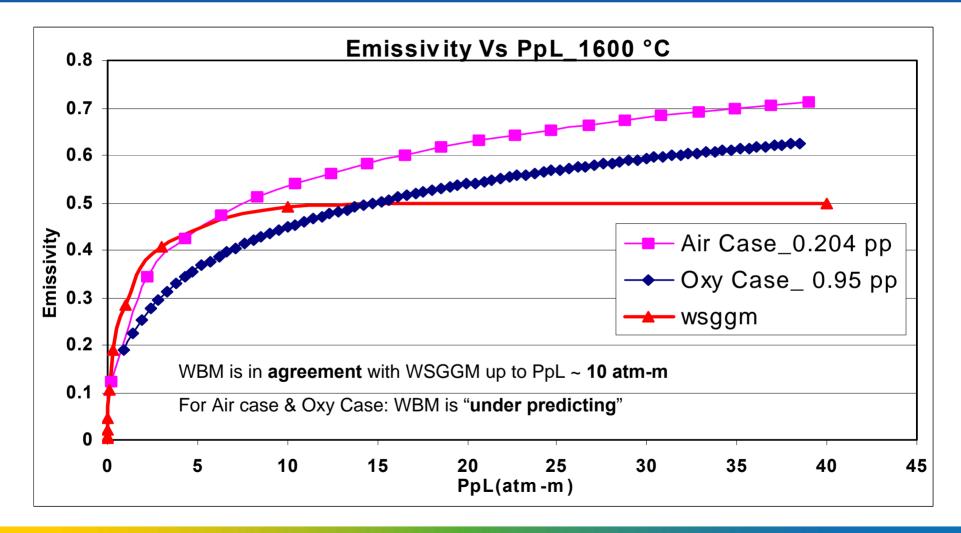
© Vattenfall AB

Lars Stromberg 2004

Source Raj Gupta, U of Newcastle, Australia

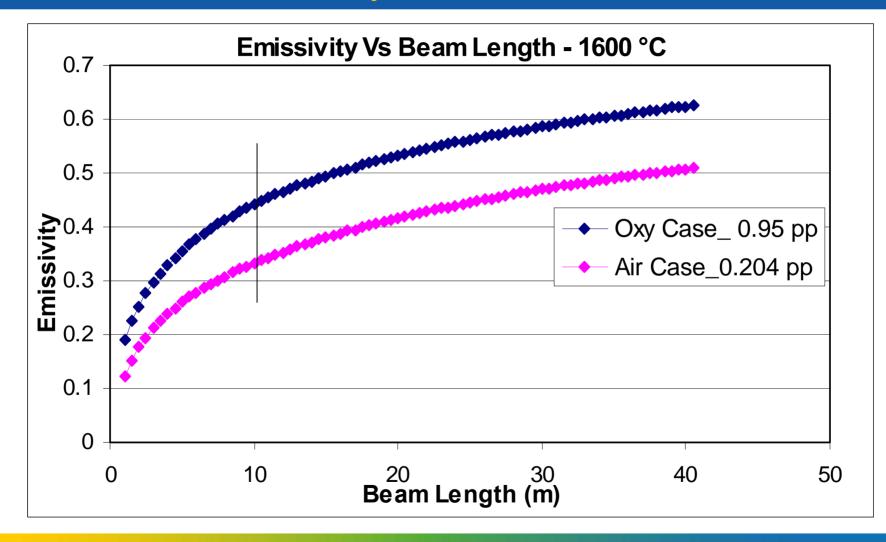


#### 55 WBM vs WSGGM Model for PpL @ 1600 °C





## 56 WBM – Air vs. Oxy Case for BL - 1600 °C



© Vattenfall AB

Source Raj Gupta, U of Newcastle, Australia



## CO<sub>2</sub> free Power Plant

15 years of research and development

Phase 0	Phase 1	Phase 2	Phase 3	Phase 4	
Is it possible?	GAP-analysis	Concept development	Technology development/ engineering	Construction and operation of demo plant	
2000	2001	2003	2006	2008	

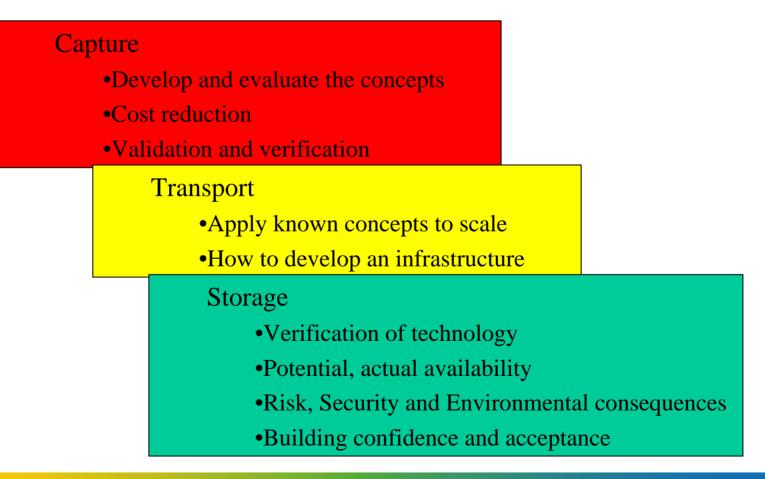
- Development target 20 €ton stored CO<sub>2</sub>
- Initial feasibility studies in 2001
- GAP analyses in 2002
- Concept development in 2003-2006
- A 250 MW electric demo-plant by latest 2010
- Commercial concept after 2015



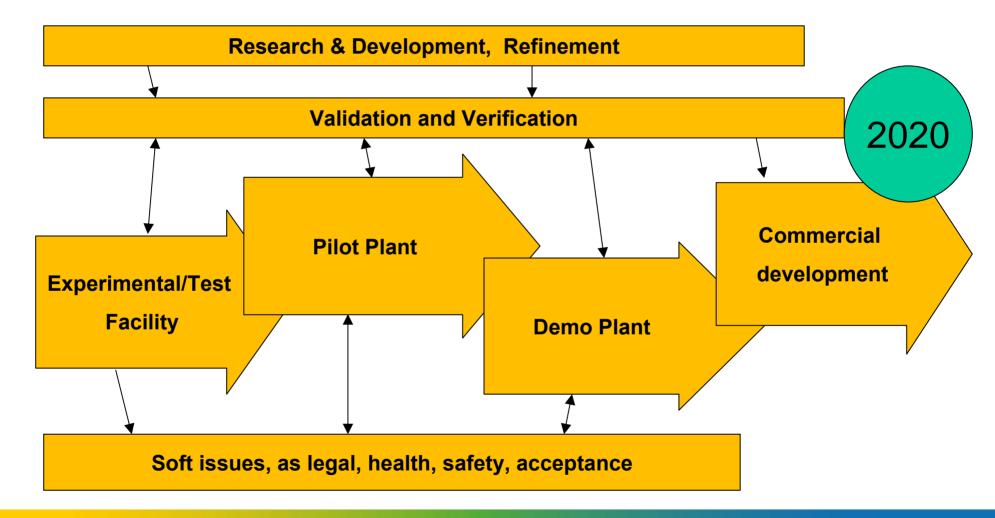
© Vattenfall AB

## <sup>58</sup> Focus of the work to reduce CO<sub>2</sub>

Focus is different for each part of the chain

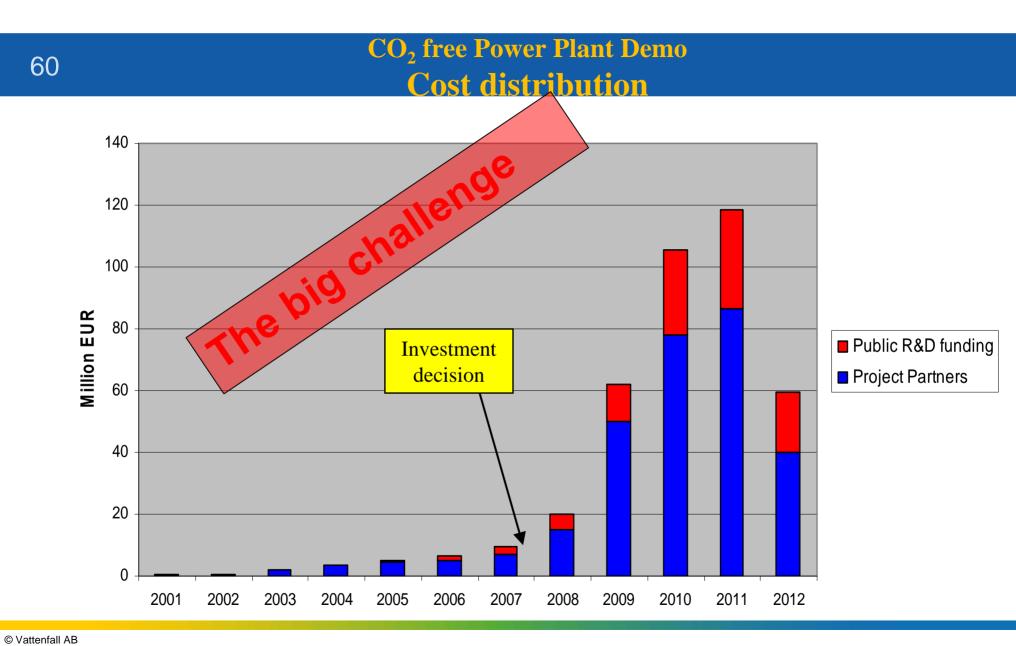


#### **CO<sub>2</sub> Free Power Plant – Work Scheme**





© Vattenfall AB





Lars Stromberg 2004

61 **CO<sub>2</sub> free power plant** 

# Conclusions



## 62 Conclusions

- Fossil fuels are needed many decades yet. There is no other option available large enough
- $CO_2$  capture and storage can enable energy generation without  $CO_2$  emissions at a lower cost than most renewable alternatives.
- The CO<sub>2</sub> emission trading scheme sets the commercial framework for new technology
- If CO<sub>2</sub> capture and storage is developed to a viable option with avoidance costs down to 20 €ton of CO<sub>2</sub>, the technology can be commercially introduced.
- "Carbon dioxide free" energy production from fossil fuels can not be introduced at a larger scale before 2015.
- Coal is competitive with gas. The commercial alternatives will be coal with CO2 capture and storage and gas without capture, taking the punishment from the trading system.



#### 63 Schwarze Pumpe power plant



