

Relaminarisation of fully turbulent pipe flow

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Numerical simulations: **Baofang Song (Tjanjin),
Burak Budanur (IST), Ashley Willis (Sheffield) and
Marc Avila (Bremen)**

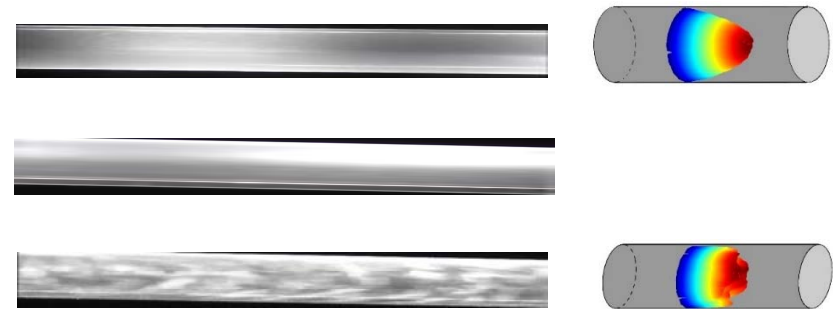
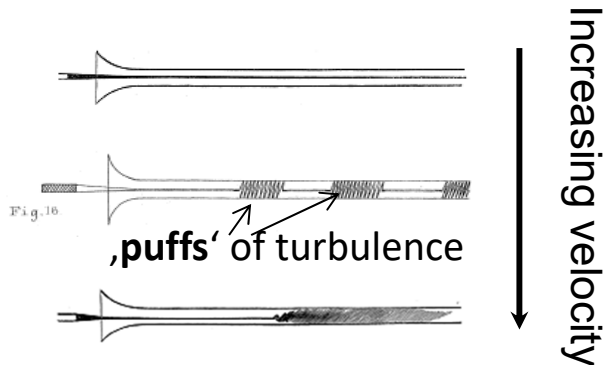
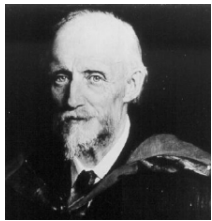


**Nonlinear Dynamics &
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Reynolds pipe experiments



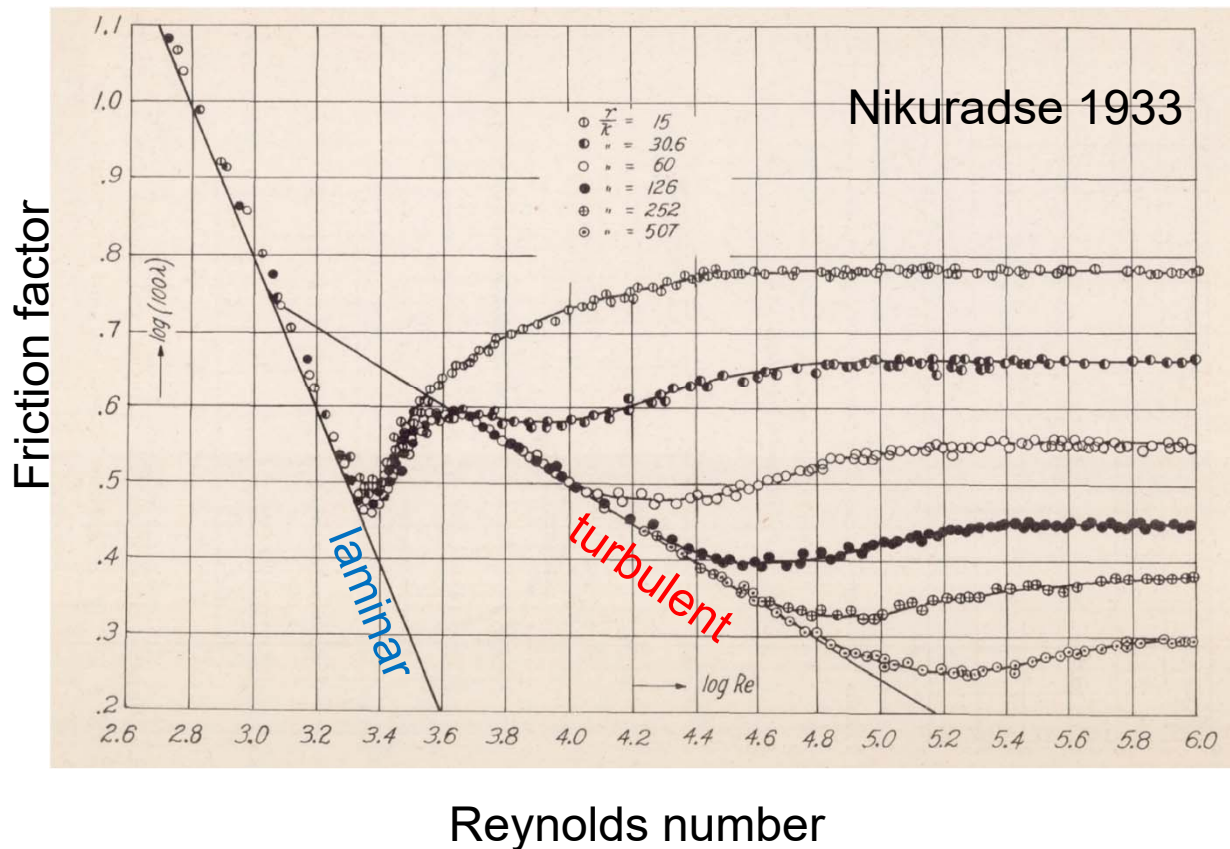
O. Reynolds Phil. Trans. R. Soc. 1883

- $Re = UD / \nu = \text{velocity} \times \text{diameter} / \text{kin. viscosity} \sim \text{inertial} / \text{viscous forces}$
Reynolds number is the **only** parameter of the problem
small $Re \rightarrow$ laminar flow
large $Re \rightarrow$ turbulence

However: transition usually occurred at $Re=2000$, but for an improved set up at $Re=13\,000$

Laminar flow is linearly stable

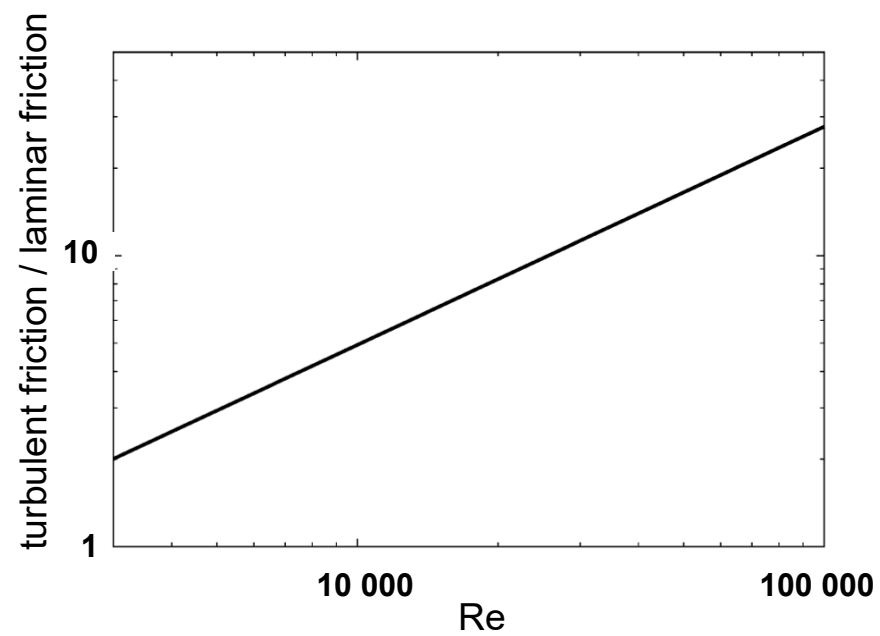
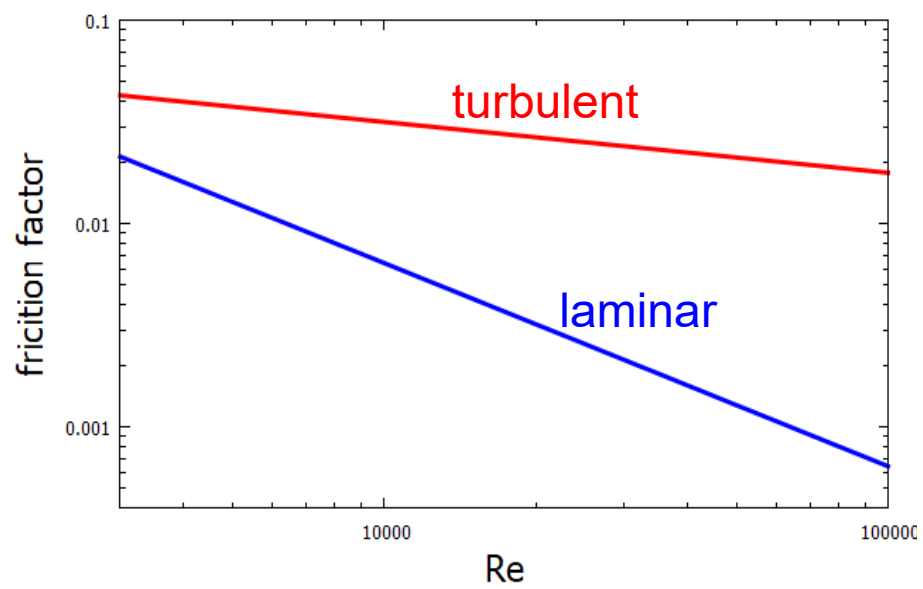
Friction in pipes



$$\Delta p = f \rho U^2 L / (2 D)$$

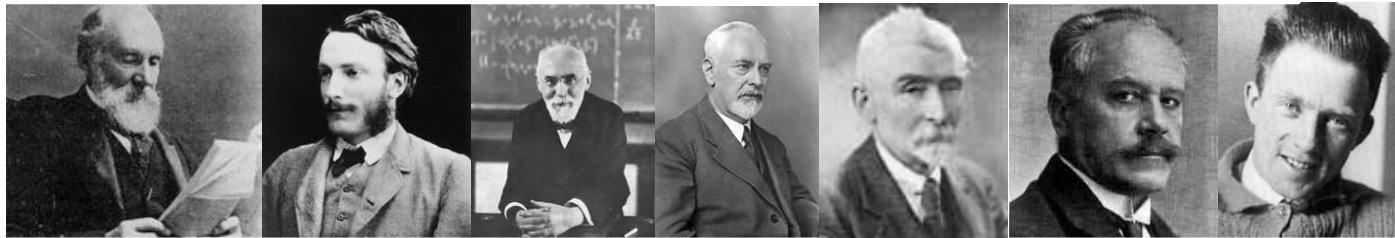
Laminar flow: $f \sim 1/Re$ $f \sim U$

Turbulent flow: $f \sim 1/Re^{-0.25}$ $f \sim U^{1.75}$



The onset of turbulence

Can we define a critical point for transition?



Kelvin

Rayleigh

Lorentz

Prandtl

Orr

Sommerfeld

Heisenberg

Prandtl (1921): "...and so, once more, we do not obtain a critical Reynolds number. There seems to be a very nasty devil in the turbulence so that all mathematical efforts are doomed to failure."

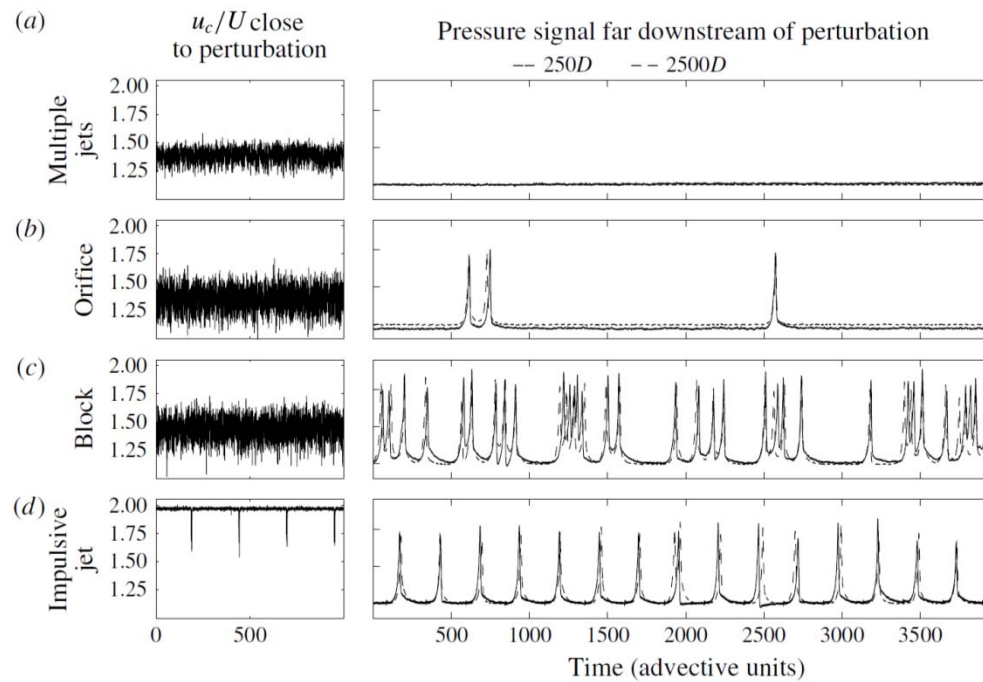
O. Reynolds Phil. Trans. R. Soc. Lond. A 174 1883

... , it became clear to me that if in a tube of sufficient length the water were at first admitted in a high state of disturbance, then as the water proceeded along the tube the disturbance would settle down into a steady condition, which condition would be one of eddies or steady motion, according to whether the velocity was above or below what may be called the real critical value.

Experimental difficulties

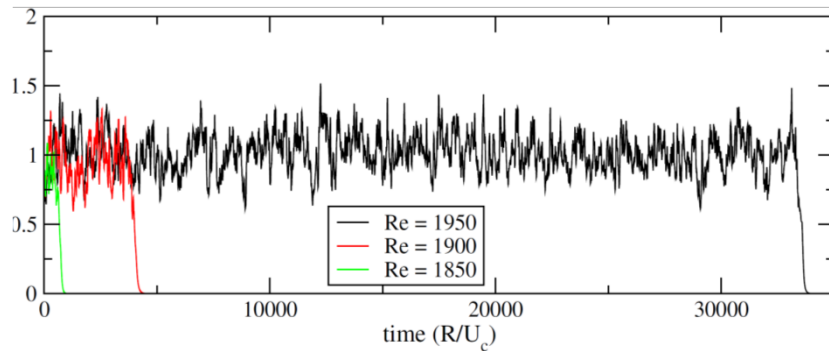
Dependence on
perturbation: (a)

Re=2100



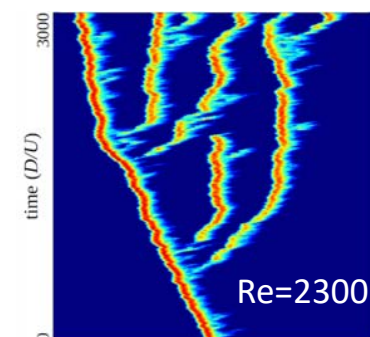
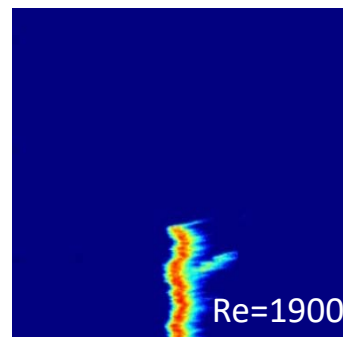
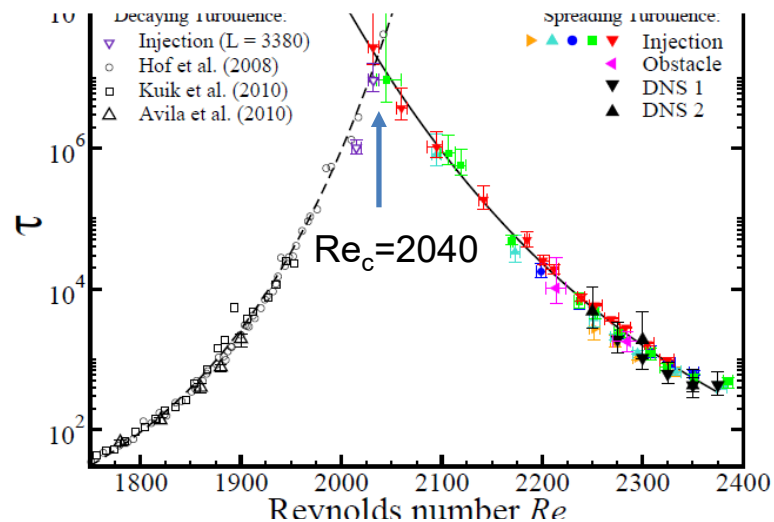
Dynamics of individual puffs

Decay of turbulent puffs



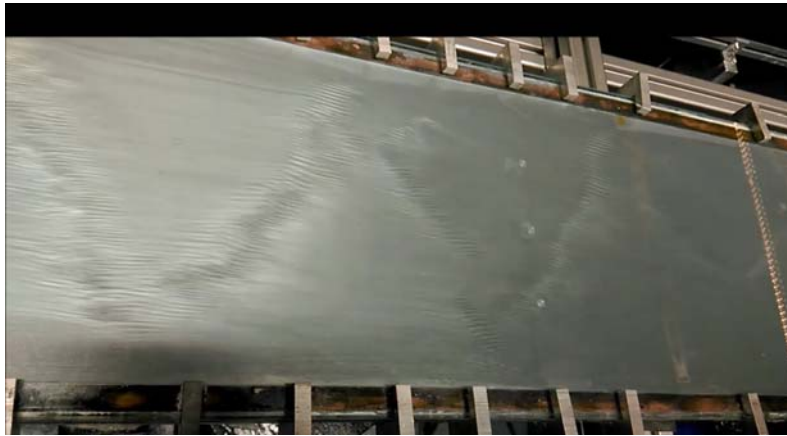
- Turbulent puffs decay suddenly after long times
- Memoryless process

$$P(t, Re) = \exp(-t / \tau(Re))$$



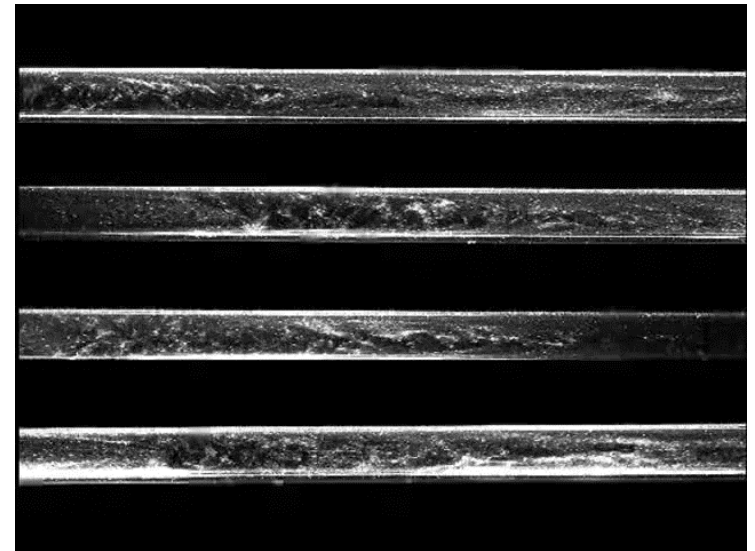
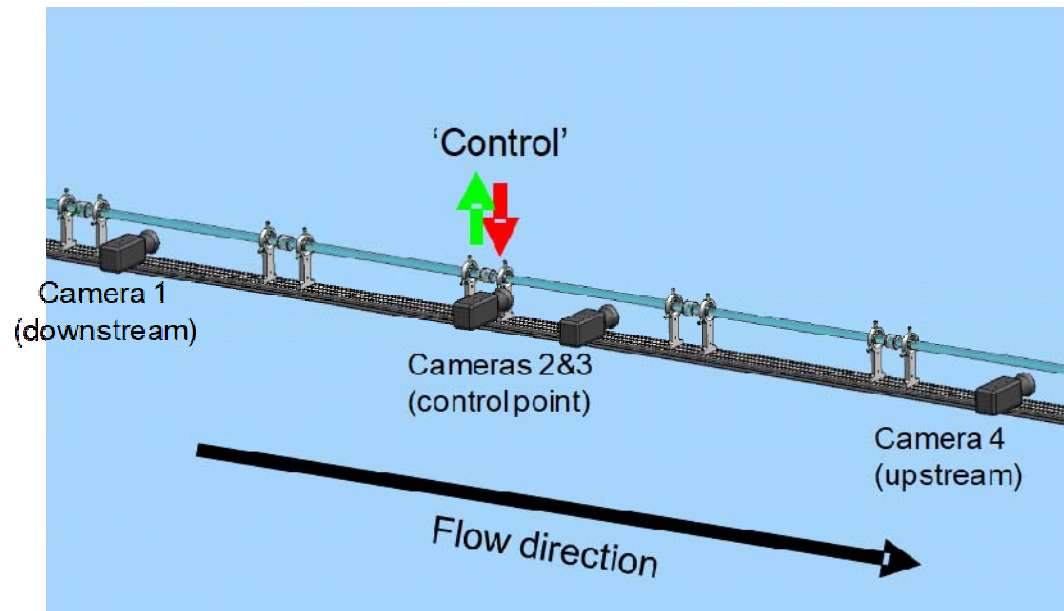
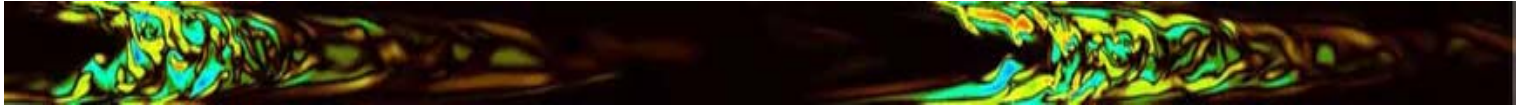
(Avila, Moxey, de Lozar, Avila, Barkley, Hof, *Science* 2011)

Transition (in Couette flow) belongs to the „**directed percolation**“ **universality class** (Lemoult et al. *Nature Physics* 2017)



Why is turbulence localised?

Puff interactions



Hof, deLozar, Avila, Tu, Schneider Science 2010

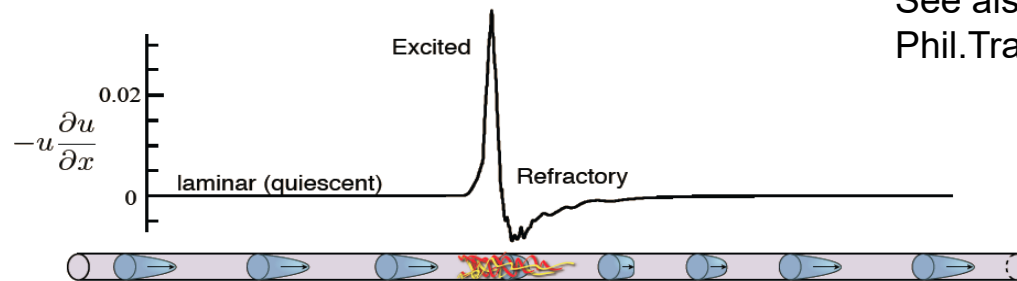
A different frame of reference

DNS by Baofang Song and BH

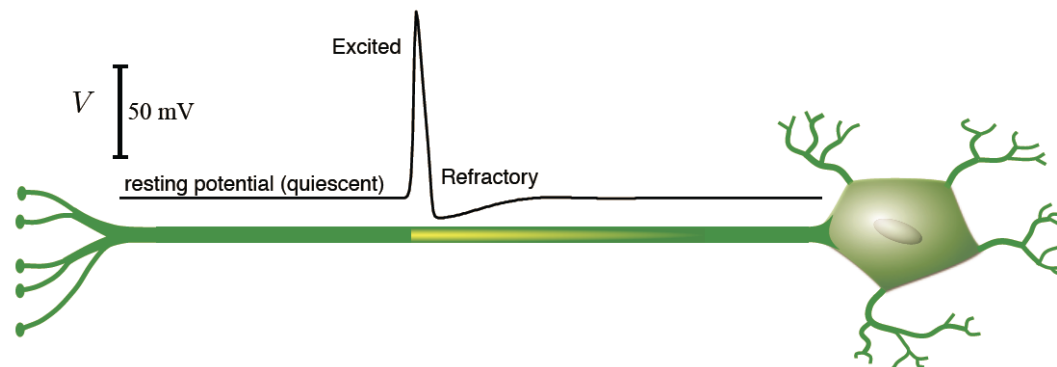


Refractory region

Puffs are 'parasites' that feed on the upstream laminar flow.

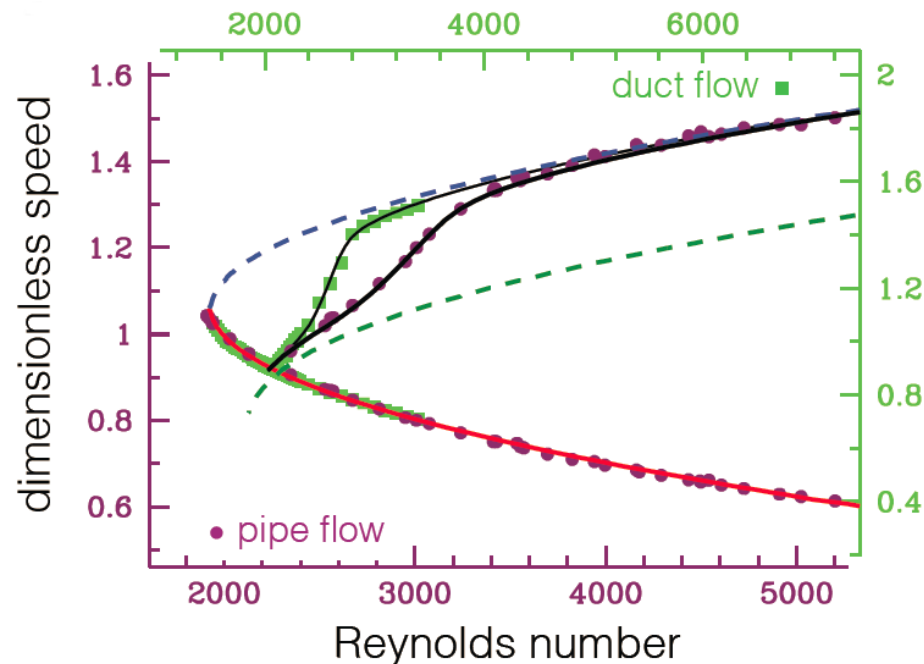
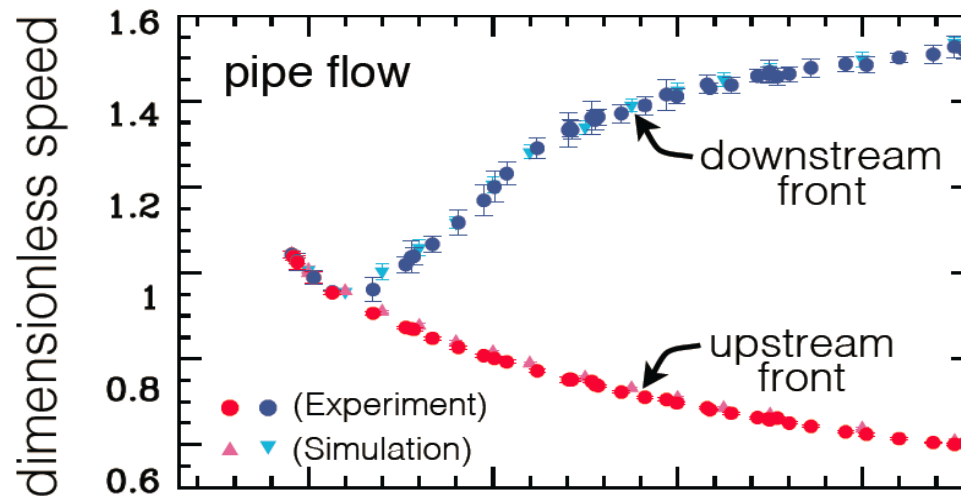


See also van Doorne and Westerweel
Phil.Trans.Roy.Soc. 2009



Barkley PRE 2011
Barkley JFM 2017

Laminar Turbulent fronts

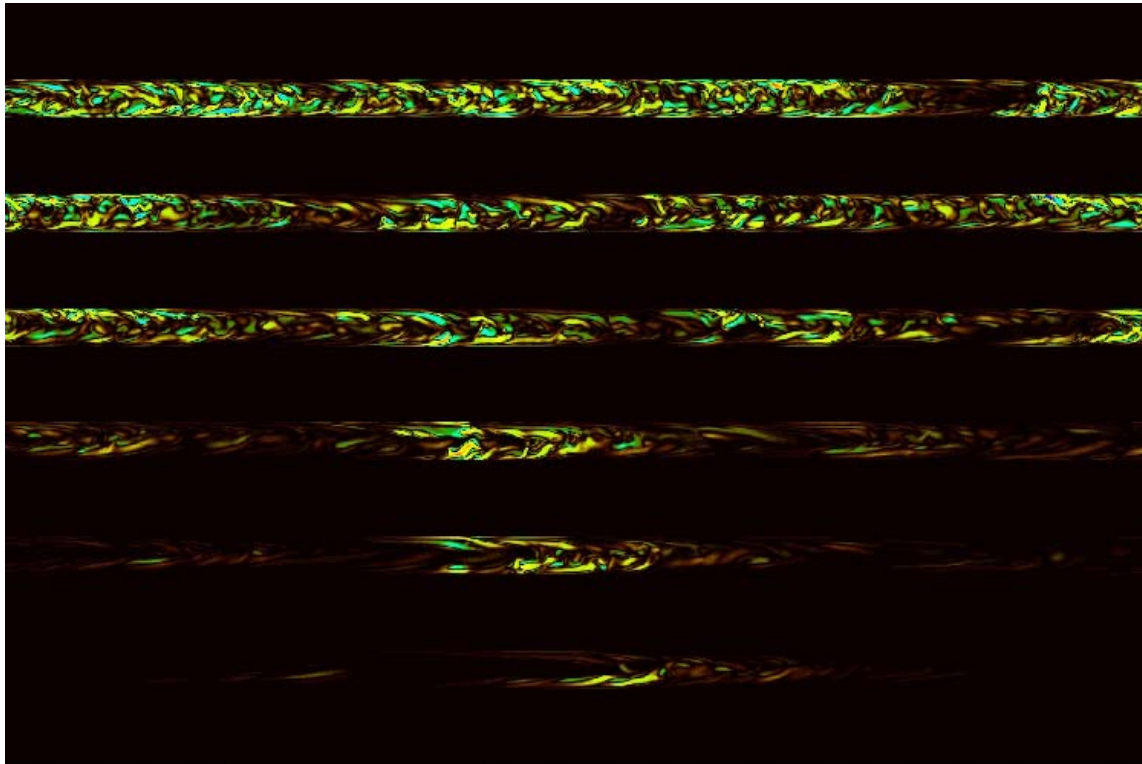


Barkley, Song, Mukund, Lemoult, Avila & Hof
Nature 2015

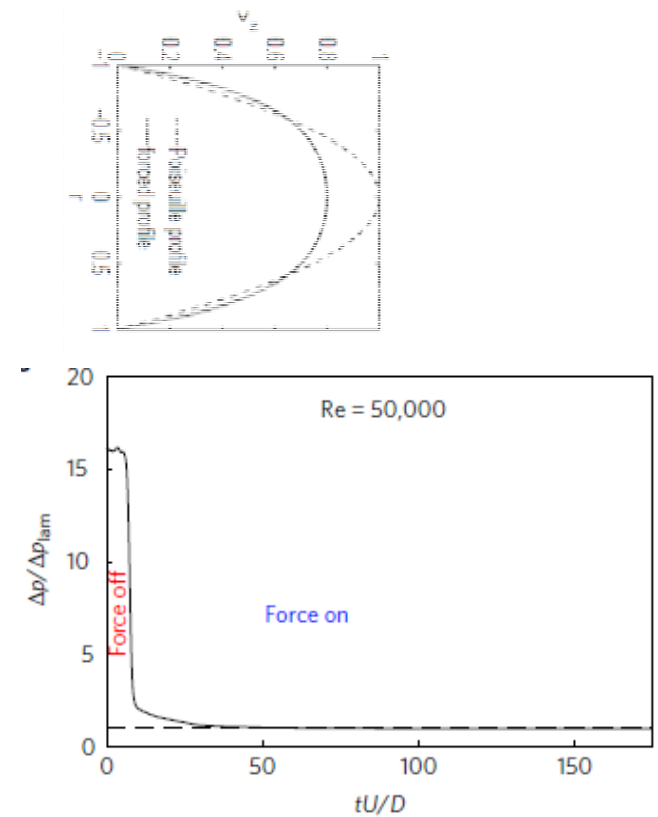
Prediction: **Profile change can make fully turbulent flow refractory**

Relaminarization in direct numerical simulations

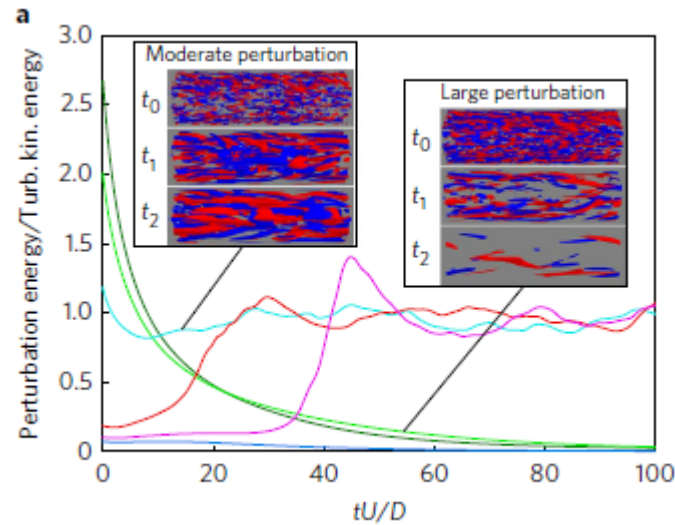
DNS pipe flow by Marc Avila: Flow relaminarizes if profile is flattened



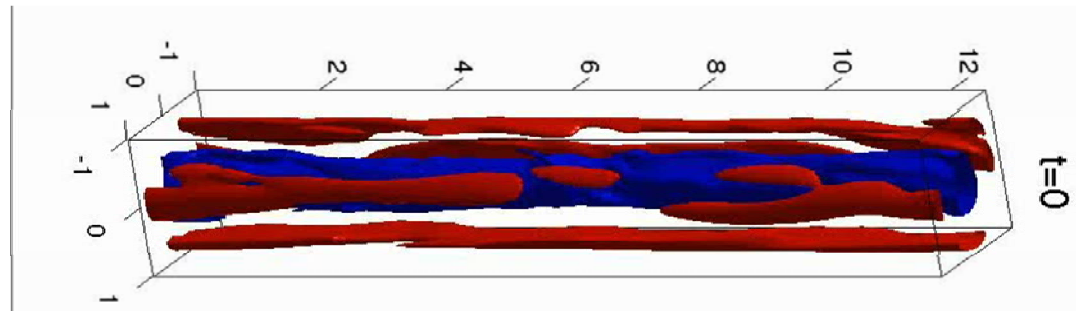
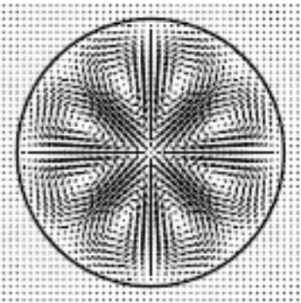
(see also Hof et al. Science 2010)



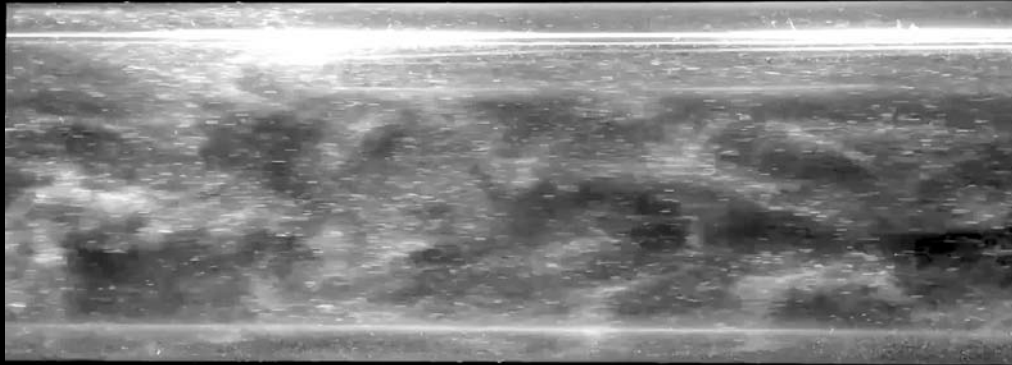
Making the flow more turbulent



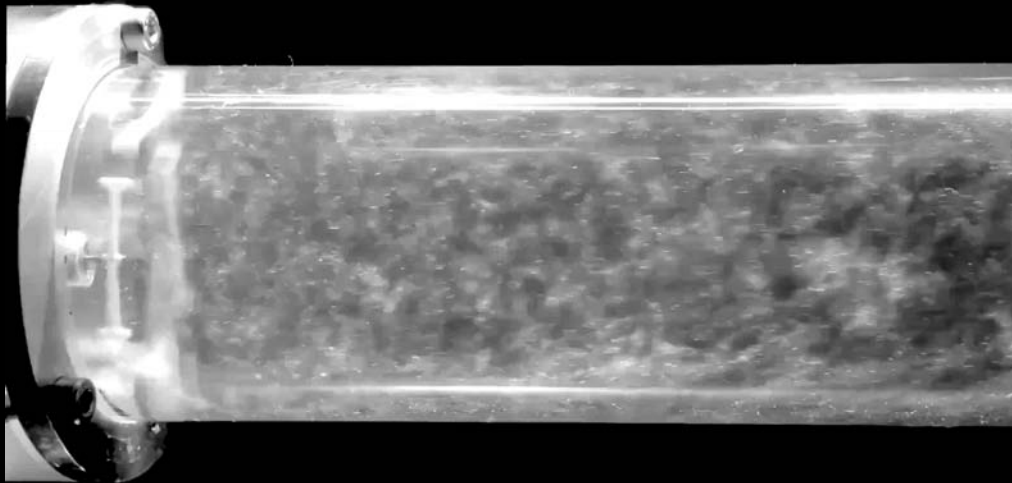
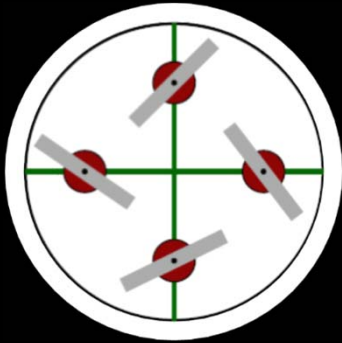
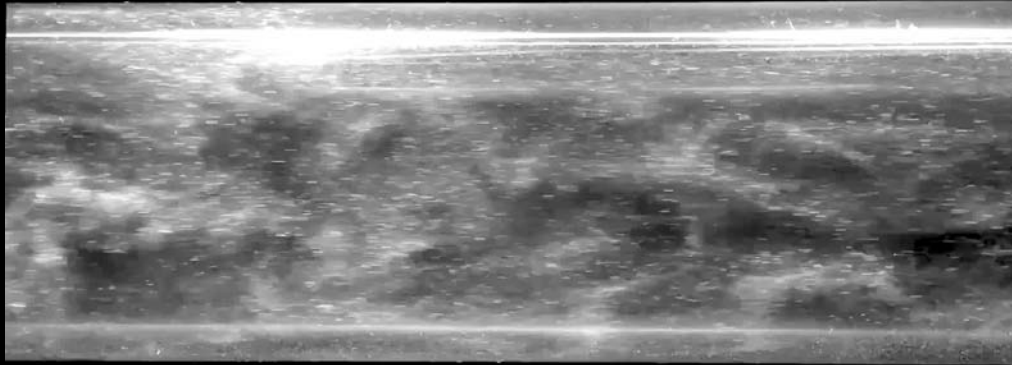
DNS by Baofang Song and Burak Budanur



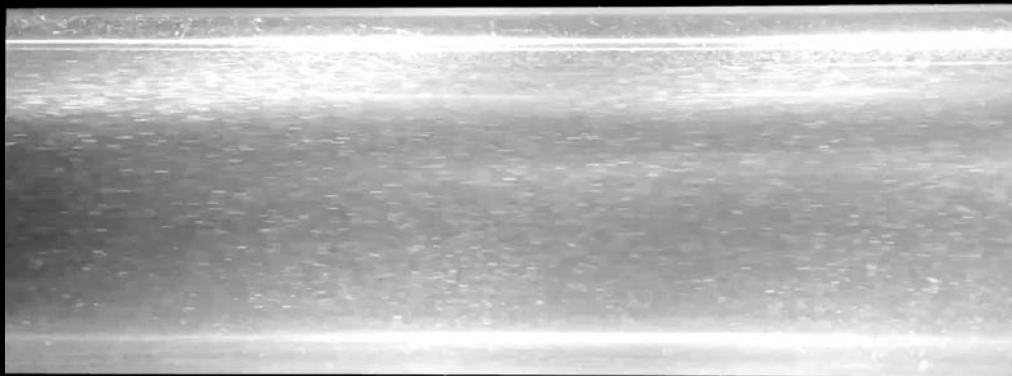
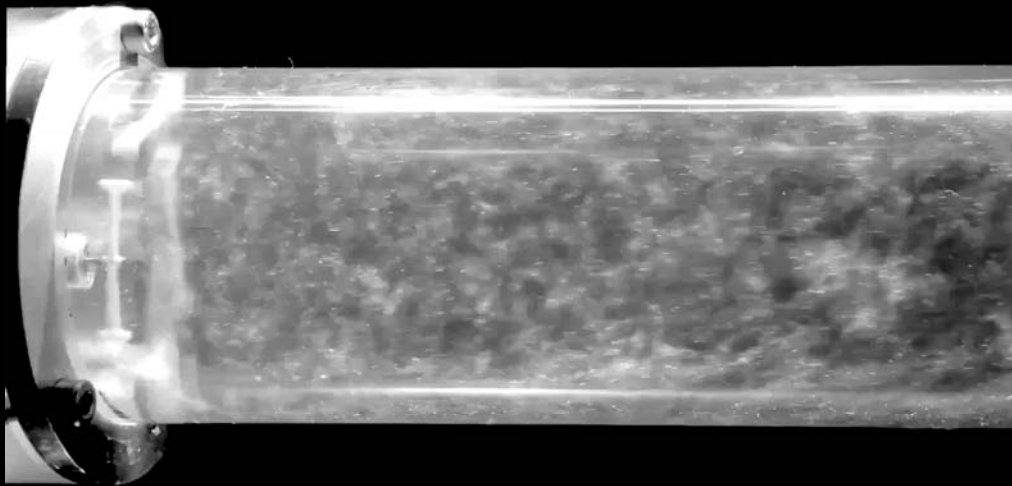
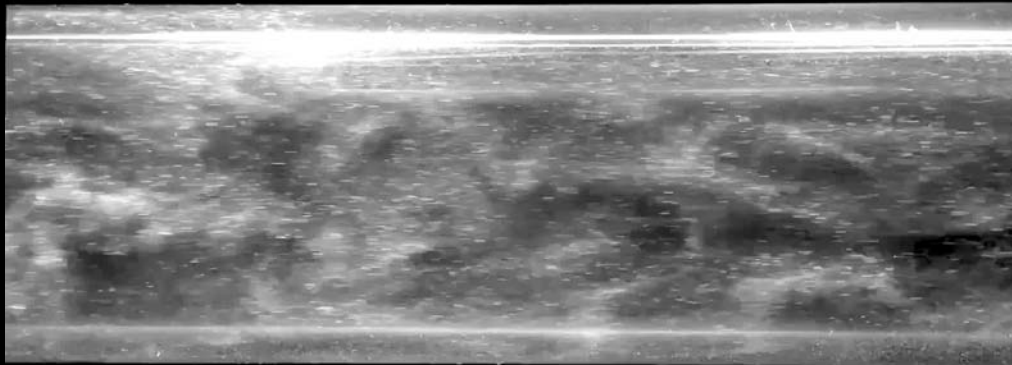
Re=3500

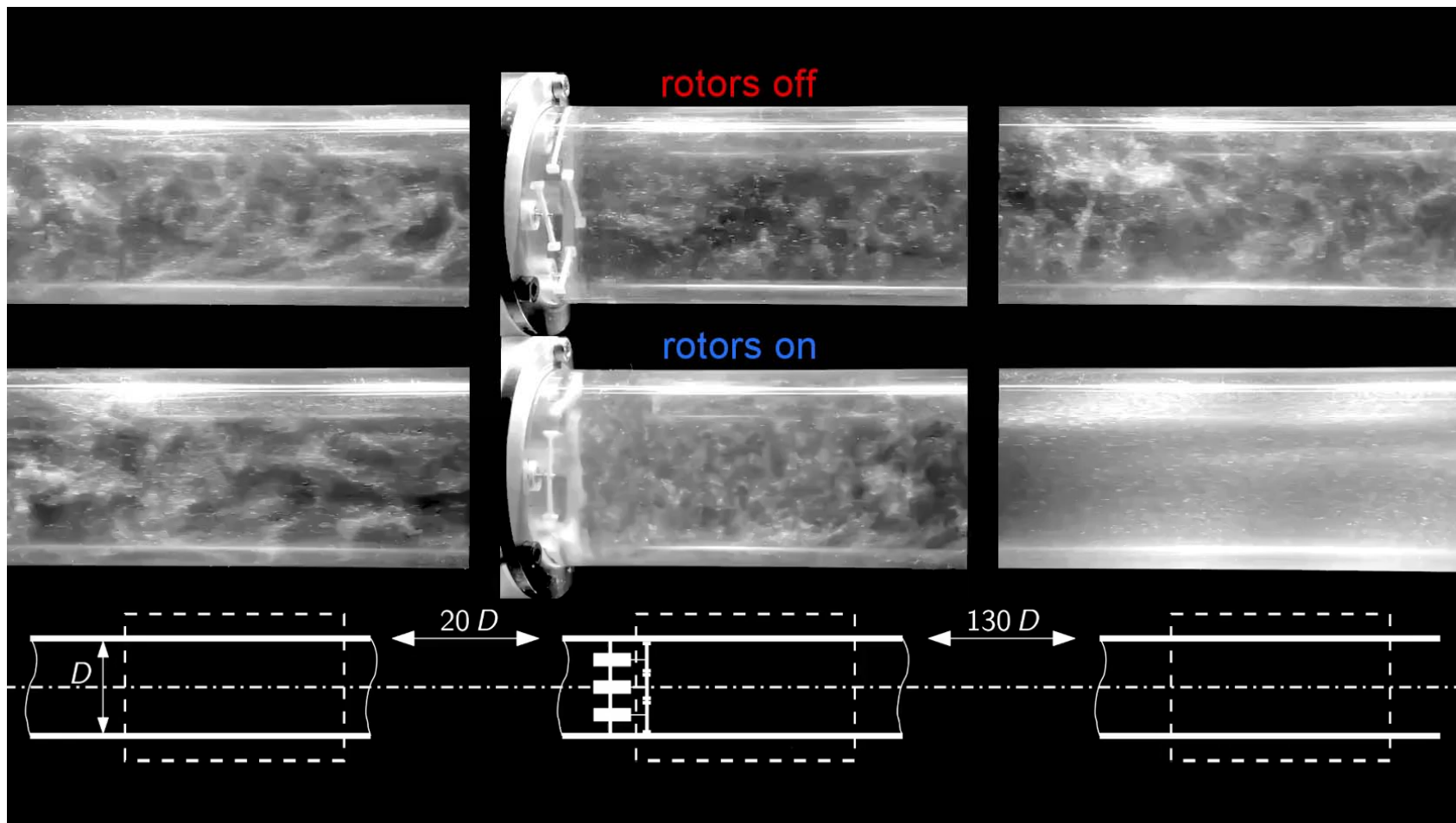


Re=3500

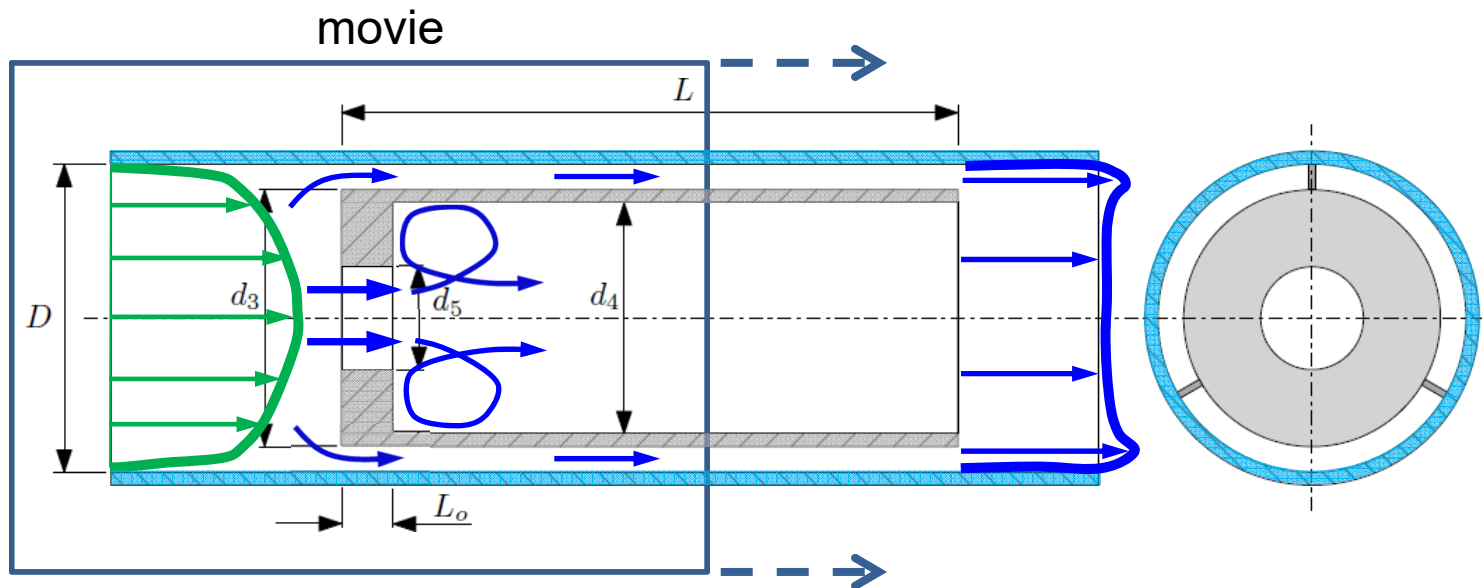


$Re=3500$





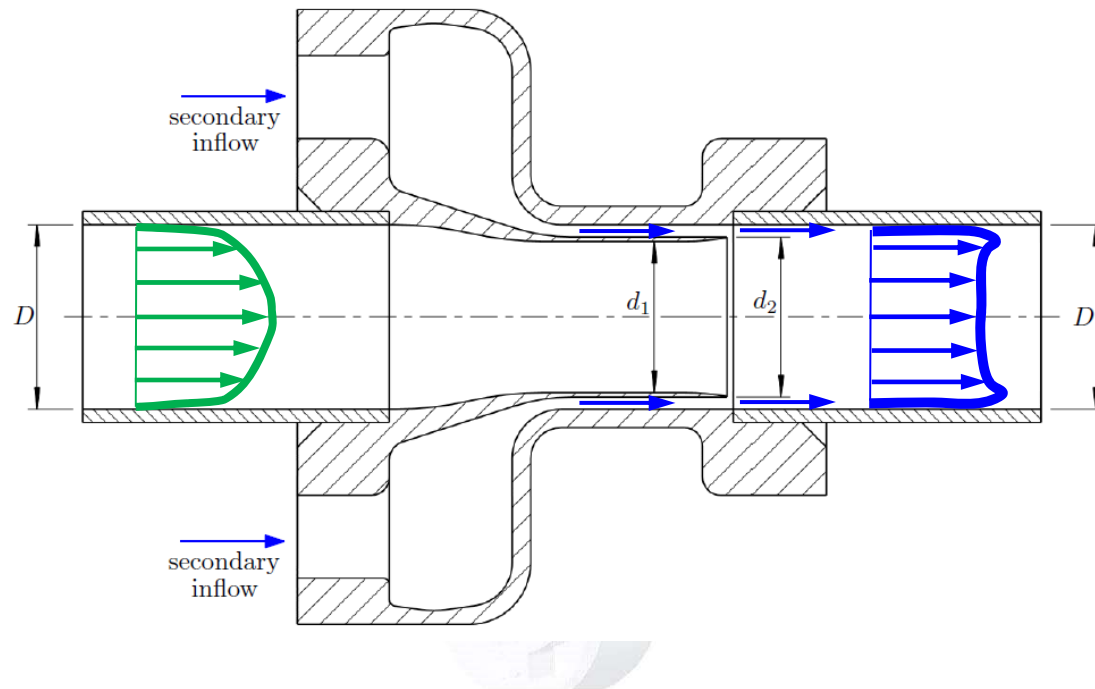
Passive device: mechanism



$Re = 4000$, camera comoving with bulk velocity of the flow



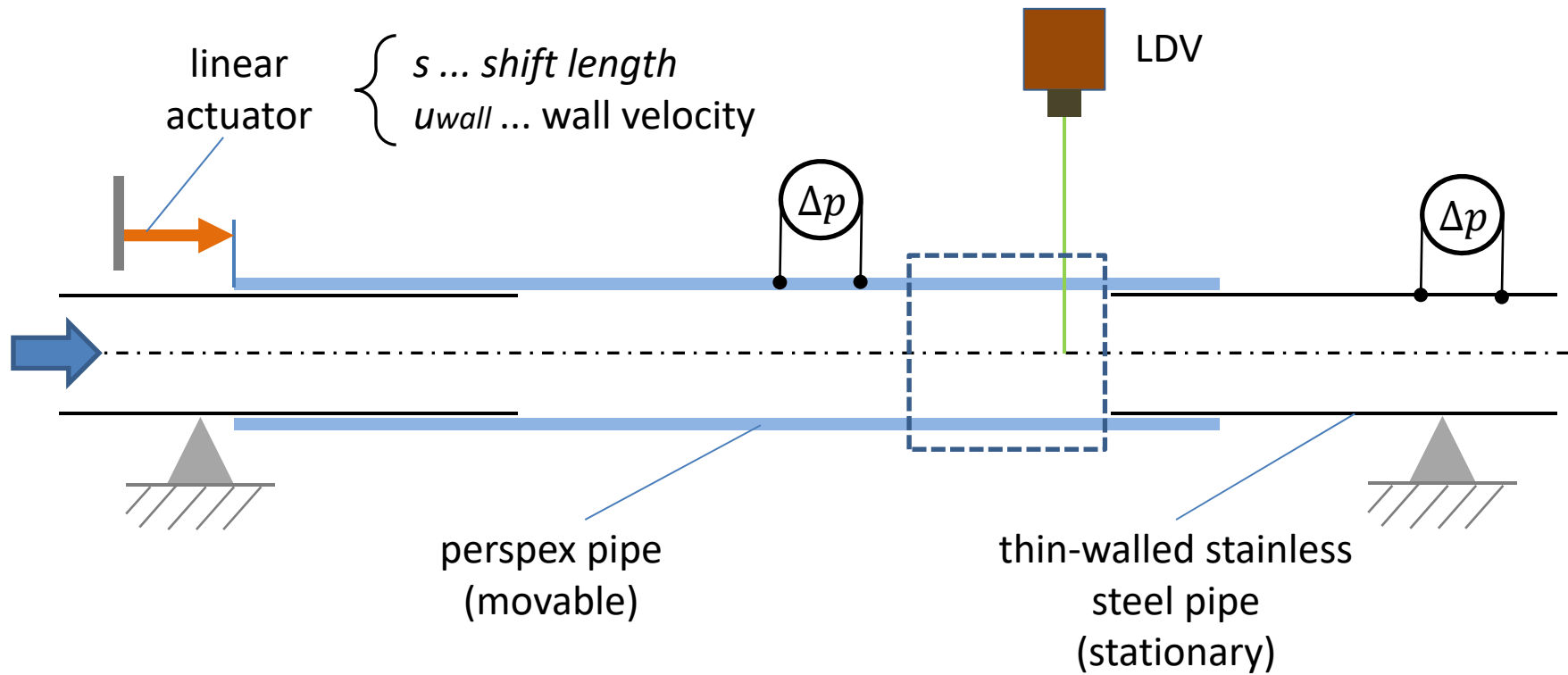
Injection through a radial gap: mechanism



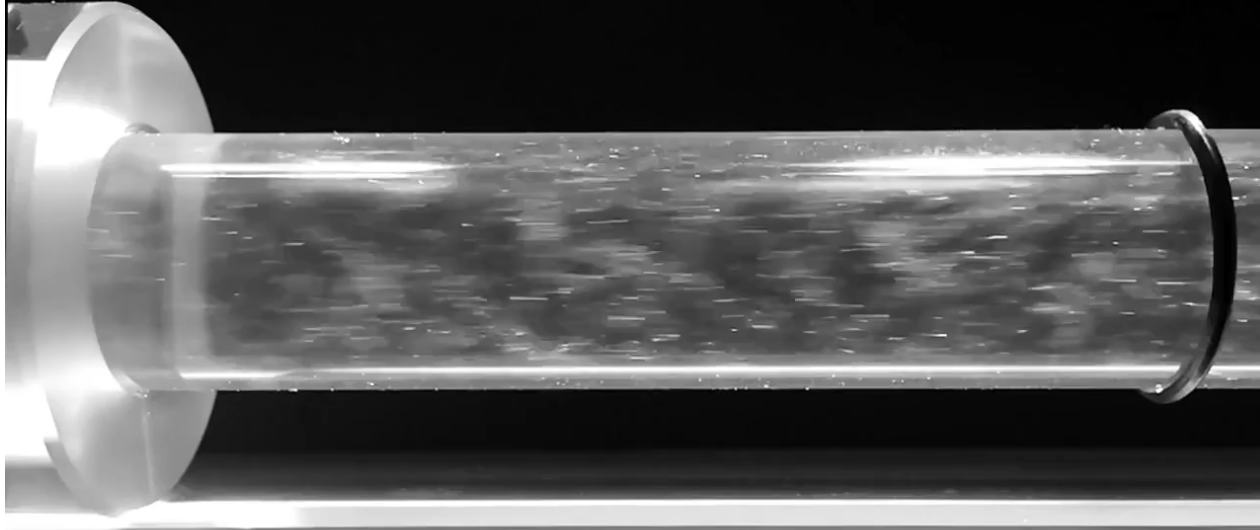
Re = 5000, injection off-on



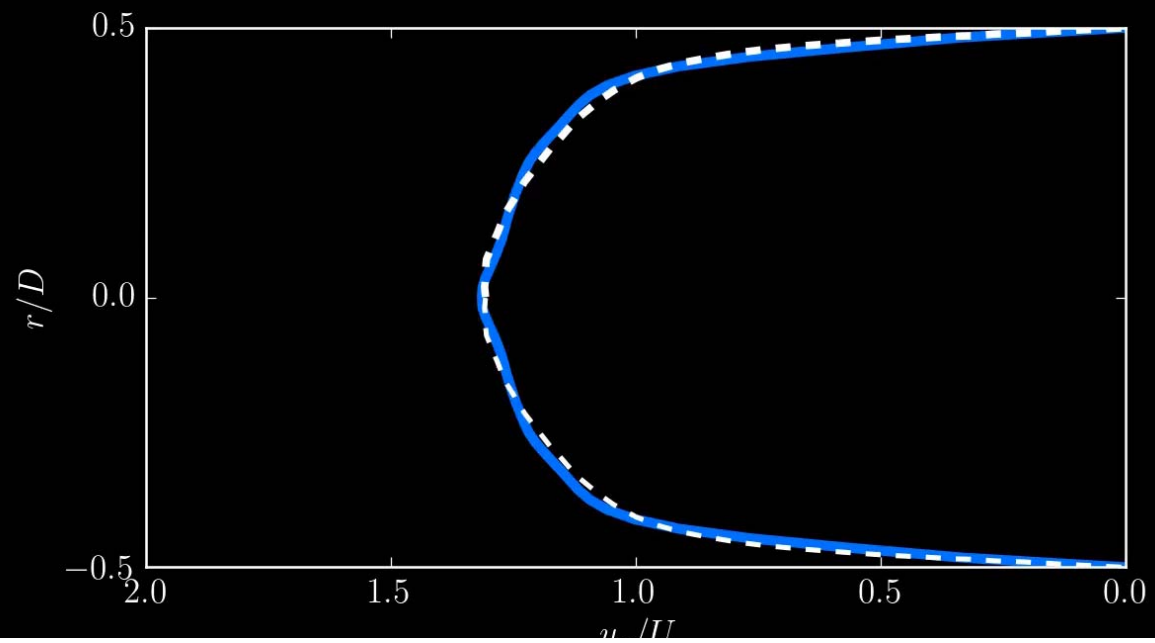
Shifting wall: control mechanism



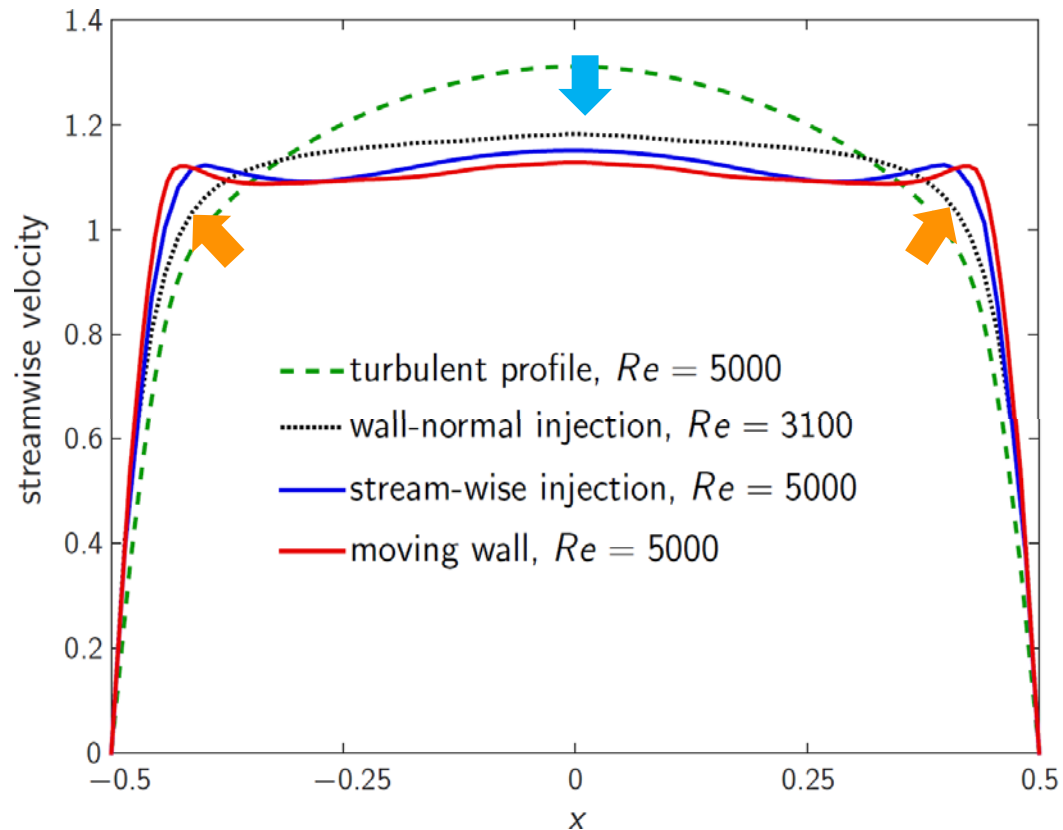
Re = 5000, video in slow-motion (25% of original speed)



Wall at rest



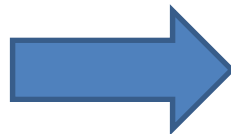
Common feature of all control mechanisms



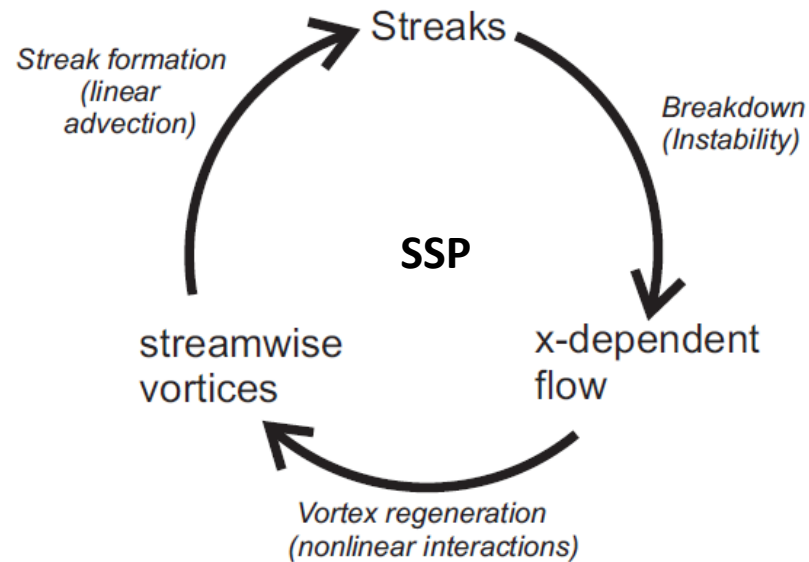
streamwise velocity profile more flat/blunt due to
⇒ increased turbulence intensity and/or
⇒ incr. velocity at the wall/decr. vel. in the center
⇒ **steeper gradient at the wall, increased friction**

The self sustaining process

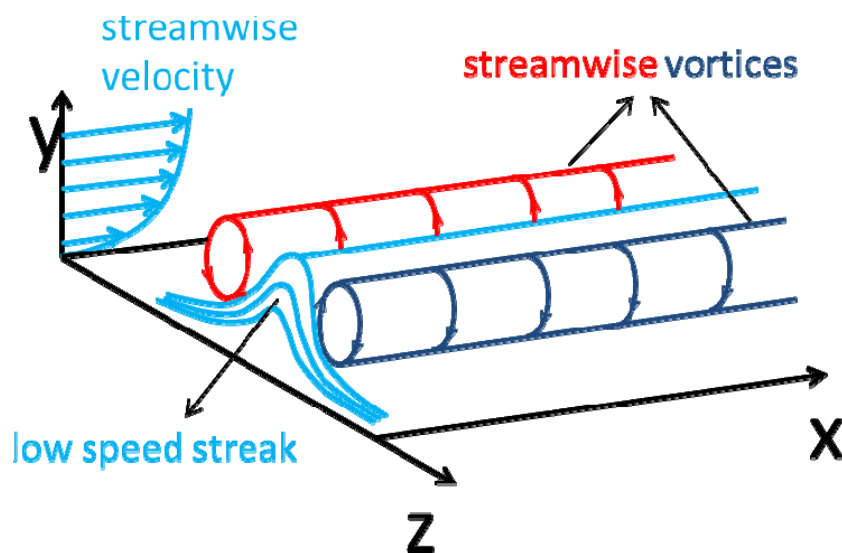
Lift up mechanism
transient growth



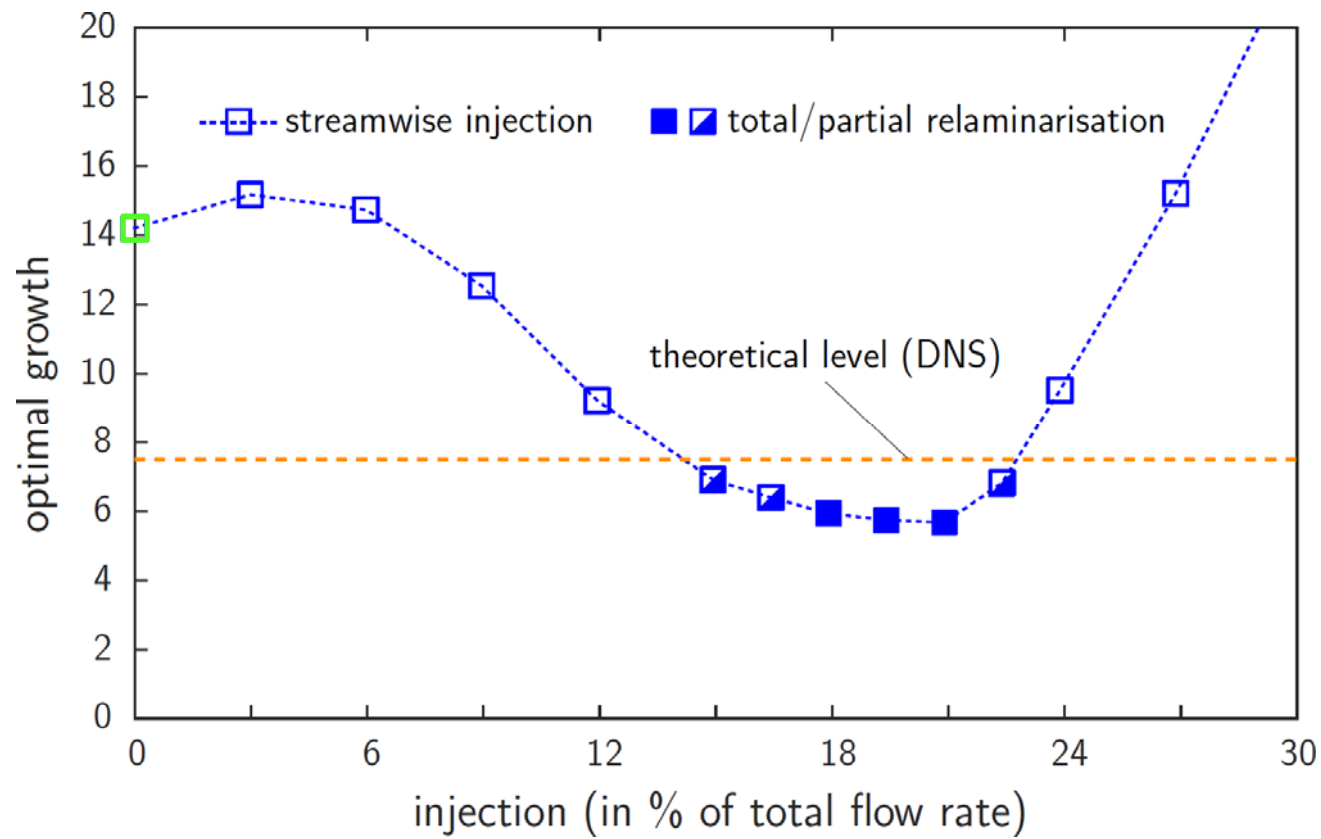
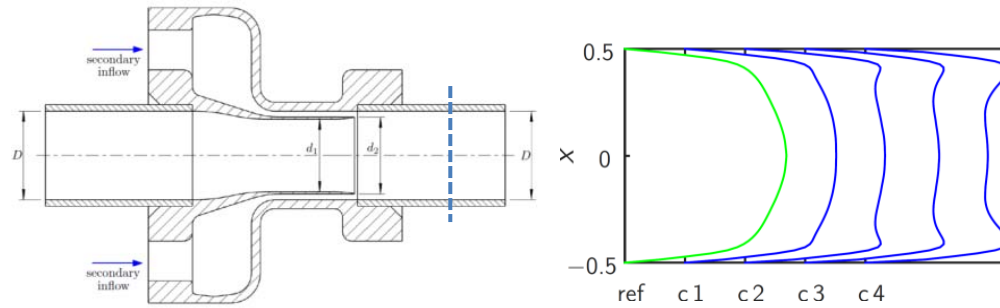
See e.g. Brandt E.J.Mech. B/Fluids 2014,
Reddy&Henningson JFM 1993,
Trefethen et al. Science 1994....



Hamilton, Kim, Walleffe JFM 1995



Transient/optimal growth



Drag reduction

