Novel approach of advanced characterization, dedicated synthesis and theoretical modelling on commercially relevant Fischer-Tropsch catalysts for production of sustainable fuels & chemicals: Bridging industry and academia



Catalyst Research for Sustainable Kerosene

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Power to Liquids process: production of sustainable aviation fuels (SAF)





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Paul B. Webb, Ivo A.W. Filot, Promoted Fischer-Tropsch catalysts in Comprehensive Inorganic Chemistry III (Third Edition), Editor(s): Jan Reedijk, Kenneth R. Poeppelmeier, Elsevier, 2023



Power from renewable sources

Production of green hydrogen

Carbon dioxide e.g. from industrial processes or direct air capture

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synthetic sustainable aviation fuels (SAF)

CARE-O-SENE: Work Packages & Partner Involvement

WP1

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characterisation and modelling



WP3 SCALE-U DEMONS FT catalys production at larger so and testing

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WP3 SCALE-UP AND DEMONSTRATION FT catalyst production at larger scale and testing



HZB Helmholtz Zentrum Berlin



CATALYST SYNTHESIS Lab scale synthesis and testing

SASOL I Fraunhofer IKTS HZB Helmholtz Zentrum Berlin

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sasol 💑

WP4 IMPACT ANALYSIS Assessment of the benefits of the FT catalyst

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Why do we need *in-situ* studies?



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- Oxidation and reduction
- Identification of the promoter structure
- Carbide formation
- Morphological changes
- Electronic structure of active species
- Electronic structure of promoter
- Influence of support
- Understanding dynamic changes
 deactivation



K.F. Kalz, R. Kraehnert, M. Dvoyashkin, R. Dittmeyer, R. Gläser, U. Krewer, K. Reuter, J.-D. Grunwaldt, *ChemCatChem* **2017**, *9*, 17.

Or in other words: Spectroscopy while the process is running...

UV-vis spectroscopy XANES, EXAFS, XES, XRD, SAXS IR/Raman spectroscopy Mössbauer spectroscopy XPS, AES Magnetometry **Products Reactants** oxide support Need for a suitable reactor Magnetic γ IR UV-vis e X-rays field Laser light

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Operando X-ray Absorption Spectroscopy at CATACT Shining a light through catalysts in closed reactors



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A. Zimina et al., *J. Phys.: Conf. Ser.* **712**, 012019 (2016) A. Zimina et al., *Rev. Sci. Instrum.* **88**, 113113 (2017)

M. Loewert et al. React. Chem. Eng. **5**, 1071 (2020) L. Pandit et al. Chem. Methods (2022).

Fischer-Tropsch reaction over Mn promoted Co-based catalysts Bundesministerium CARE-O-SENE für Bildung und Forschung Catalyst Research for Sustainable Kerosene (5) dehydrogenation monomer CO and H_2 dissociation and CH_4 formation C₅₊ hydrocarbons $H_2 + CO$ formation Long chain formation (4) chain-reorientation CARBIDE MECHANISM (1) CH insertion Support (3) $= Co_3O_4$ (2) 3-C-hydrogenation β-C-hydrogenation = MnO₂ Co⁰ Mn²⁺

Paul B. Webb, Ivo A.W. Filot, Promoted Fischer-Tropsch catalysts in Comprehensive Inorganic Chemistry III (Third Edition), Editor(s): Jan Reedijk, Kenneth R. Poeppelmeier, Elsevier, 2023

V. Vermaak, J.H. Potgieter, E. van Steen, D.J. Moodley, M. Claeys, J.L. Visagie, R. Crous, J.M. Botha "Lift-off to sustainable aviation fuels: Optimization of Fischer-Tropsch performance with manganese promotion" CATSA 2022,13-16th November 2022, Drakensburg, South Africa

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Long-term operando studies for FTS



Re-Co/ γ -Al₂O₃ Catalyst 1:4 γ -Al₂O₃; 83,8 mg; 100-200 μ m

Conversion & C-balance



- M. Loewert, M.-A. Serrer, T. Carambia, M. Stehle, A. Zimina,,K. F. Kalz, H. Lichtenberg, E. Saraçi, P. Pfeifer and J.-D. Grunwaldt., React. Chem. Eng. 2020, **5**, 1071
- Selectivity gas-phase



- 3 regimes of deactivation
 - 1-8 h TOS: ~85 % X_{CO} to 66 %
 - 8-100 h TOS: 66 % X_{CO} to 55 %
 - 100-310 h TOS: 55 % X_{CO} to 33 %

3 regimes of selectivity

- 1-8 h TOS: ~2 % SCH4 to 7 %
- 8-60 h TOS: 7 % SCH4 to 18 %
- 60-310 h TOS: 18 % SCH4

Selectivity liquid-phase



First sample obtained after 70 h TOS
Stable product selectivity



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Operando long-term FTS – 310 h TOS

Difference Spectra

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M. Loewert, M.-A. Serrer, T. Carambia, M. Stehle, A. Zimina, K. F. Kalz, H. Lichtenberg, E. Saraçi, P. Pfeifer and J.-D. Grunwaldt., React. Chem. Eng. 2020, **5**, 1071

First Derivative









Comparison of yield/selectivity of Co- and Mn-Co-based FT catalyst





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sasol

Micro-slurry reactor (10-20g

catalyst) at industrially

relevant conditions

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How is the structure during reduction & under reaction conditions? – X-ray absorption spectroscopy



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Active state: metallic cobalt Different supports: variation in Co(II) Promoter structure: mainly Mn²⁺, nonstoichiometric

Reduction behavior: support dependent, reduction of cobalt oxide starts earlier in presence of Mn, but formation of metallic Co is retarded.

Further reduction **upon time-on-stream** (note: short reaction time), metallic Co NP growth.

In-situ magnetometry on Co/Co-Mn Fischer Tropsch catalysts



Claeys, et al, US Patent, US20110204884A1, 2009

- Support influences the magnetization degree of cobalt (lower for Alumina-based compared to Silicabased).
- Mn addition influences the Co⁰ crystallite size and retards the reduction of cobalt oxide to Co⁰.

M. Claeys, D. Moodley, JM Botha, J. Potgieter, et al. (UCT/Sasol)

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In-situ XRD on Co/Co-Mn Fischer Tropsch catalysts



- Support influences the reduction temperature and degree of cobalt oxides and final crystalline phase composition of Co⁰
- Mn addition influences the Co⁰ crystallite size, accelerates the reduction of Co_2O_3 to Co^{2+} and retards the reduction of Co^{2+} to Co^0 .

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Need for model systems to understand complex nature of catalyst



Isolation via

- Dedicated synthesis (model structures and model catalysts)
- Theoretical consideration (MSI, Co-promotor interaction)

- Wetness impregnation
- Surfactant-free benzyl-alcohol synthesis



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Unfluence of support via dedicated synthesis





Theoretical approach towards understanding promotion and support interaction via DFT

Metal-Support-Interaction: solid phase formation

🔵 Co 🔘 Al 🕒 O



Metal-Promoter-Interaction: Size dependence







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Structure of promoter

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Deactivation of Co-based Fischer-Tropsch catalysts

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Solid-State Reaction Morphologial Changes Active State Fore Blocking Sintering Oxidation Oxidation Sintering Oxidation Oxidation Sintering Oxidation Oxidation Sintering Oxidation Sintering Oxidation Oxidation Sintering Oxidation Oxidation Sintering Oxidation Oxidation Sintering Oxidation Oxidation Oxidation Sintering Oxidation Oxidation Oxidation Sintering Oxidation Oxidation Sintering Oxidation Oxidation Oxidation Sintering Oxidation Oxidation Oxidation Oxidation Oxidation Sintering Oxidation Oxi

Pore blocking

Interface formation

Carbon deposition

Catalytic testing Spectroscopic methods Imaging methods

Conclusions and outlook

- On the way of bridging the gap between industrially applied catalysts and studies at the synchrotron
 - Characterization under industrial relevant conditions on commercial relevant materials demanding (but possible)
 - Fouling processes are critical for deactivation
 - Multimodel and multiscale approach required for characterization
 - Dedicated synthesis of defined model systems and theoretical considerations
- Know-how transfer to the CARE-O-SENE Project: interdisciplinary, institutional and international collaborative project for long term cooperation in the field of sustainable catalysis
 - Improved understanding and development of PtL catalysts for sustainable kerosene
 - XAS studies: catalyst behavior and deactivation phenomena
 - Theory: knowledge-based design of catalysts, understanding of reaction dynamics and deactivation mechanics
 - Next steps: Hard and soft XAS, extension to imaging methods

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